

Manahan, Stanley E. "INDUSTRIAL ECOLOGY FOR WASTE MINIMIZATION, UTILIZATION,  
AND TREATMENT

*Fundamentals of Environmental Chemistry*

Boca Raton: CRC press LLC, 2001

## 22 INDUSTRIAL ECOLOGY FOR WASTE MINIMIZATION, UTILIZATION, AND TREATMENT

---

---

### 22.1 INTRODUCTION

Chapter 21 addressed the nature and sources of hazardous wastes and their environmental chemistry and pointed out some of the major problems associated with such wastes. Chapter 22 deals with means for minimizing wastes, utilizing materials that might go into wastes, and treating and disposing of wastes, the generation of which cannot be avoided. The practice of industrial ecology combined with green chemistry is all about not producing wastes and, instead, utilizing wastes for useful purposes. Therefore, in dealing with wastes, it is essential in the modern age to consider the potential contribution of industrial ecology.

Since the 1970s, efforts to reduce and clean up hazardous wastes have been characterized by:

- Legislation
- Regulation
- Litigation
- Procrastination
- Modeling
- Analysis
- Cleanup of a few select sites

It is perhaps fair to say that in proportion to the magnitude of the problems and the amount of money devoted to them so far, insufficient progress has been made in coping with hazardous wastes. In the U.S., huge amounts of time have been devoted to promulgating hazardous-waste regulations, instrument manufacturers have prospered as more and more chemical analyses have been required, and computationists, some of whom would be offended at the sight of any chemical, much less a hazardous one, have consumed thousands of hours of computer time to model hazardous-waste systems. This is to say nothing of the vast expense of litigation that has gone into lawsuits dealing with hazardous-waste sites. In the future, a higher percentage of

the effort and resources devoted to hazardous wastes needs to be placed on remediation of existing problems and preventive action to avoid future problems.

The U. S. Superfund act, a particular target of criticism by industrial and other groups, has been under consideration for renewal each year since 1994. A total of nine bills dealing with Superfund were introduced in the U.S. Congress in 1999, none with much of a chance of passing.<sup>1</sup> Critics contend that Superfund's efforts have been directed toward high-cost solutions for minimal risks. Many Superfund critics contend that a much greater emphasis must be placed on institutional controls and waste isolation to deal effectively with improperly disposed hazardous wastes.

This chapter discusses how environmental chemistry can be applied to hazardous-waste management to develop measures by which chemical wastes can be minimized, recycled, treated, and disposed. In descending order of desirability, hazardous-waste management attempts to accomplish the following:

- Do not produce it
- If making it cannot be avoided, produce only minimum quantities
- Recycle it
- If it is produced and cannot be recycled, treat it, preferably in a way that makes it nonhazardous
- If it cannot be rendered nonhazardous, dispose of it in a safe manner
- Once it is disposed, monitor it for leaching and other adverse effects

The **effectiveness** of a hazardous-waste management system is a measure of how well it reduces the quantities and hazards of wastes. As shown in [Figure 22.1](#), the best management option consists of measures that prevent generation of wastes. Next in order of desirability is recovery and recycling of waste constituents, followed by destruction and treatment with conversion to nonhazardous-waste forms. The least desirable option is disposal of hazardous materials in storage or landfill.

## 22.2 WASTE REDUCTION AND MINIMIZATION

The initial sections of this chapter address waste reduction and minimization. During recent years, substantial efforts have been made toward reducing the quantities of wastes and, therefore, the burden of dealing with wastes. Much of this effort has been the result of legislation and regulations restricting wastes, along with the resulting concerns over possible legal actions and lawsuits. In many cases—and ideally in all—minimizing the quantities of wastes produced is simply good business. Wastes are materials, materials have value and, therefore, all materials should be used for some beneficial purpose and not discarded as wastes, usually at a high cost for waste disposal.

Industrial ecology is all about the efficient use of materials. Therefore, by its nature, a system of industrial ecology is also a system of waste reduction and minimization. In reducing quantities of wastes, it is important to take the broadest possible view. This is because dealing with one waste problem in isolation may simply create another. Early efforts to control air and water pollution resulted in

problems from hazardous wastes isolated from industrial operations. A key aspect of industrial ecology is its approach based upon industrial systems as a whole, making a system of industrial ecology by far the best means of dealing with wastes by avoiding their production.

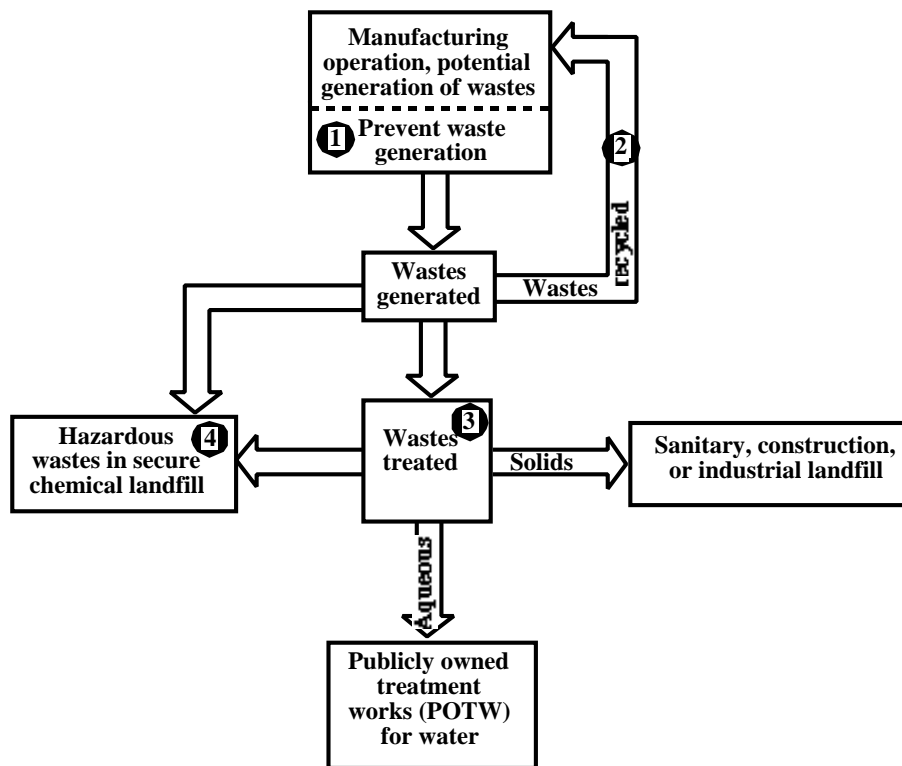


Figure 22.1 Order of effectiveness of waste-treatment management options. The darkened circles indicate the degree of effectiveness from the most desirable (1) to the least (4).

Many hazardous-waste problems can be avoided at early stages by **waste reduction** (cutting down quantities of wastes from their sources) and **waste minimization** (utilization of treatment processes that reduce the quantities of wastes requiring ultimate disposal). This section outlines basic approaches to waste minimization and reduction.

There are several ways in which quantities of wastes can be reduced, including source reduction, waste separation and concentration, resource recovery, and waste recycling. The most effective approaches to minimizing wastes center around careful control of manufacturing processes, taking into consideration discharges and the potential for waste minimization at every step of manufacturing. Viewing the process as a whole (as outlined for a generalized chemical manufacturing process in [Figure 22.2](#)) often enables crucial identification of the source of a waste, such as a raw material impurity, catalyst, or process solvent. Once a source is identified, it is much easier to take measures to eliminate or reduce the waste. The most effective approach to minimizing wastes is to emphasize waste minimization as an integral part of plant design.<sup>2</sup>

Modifications of the manufacturing process can yield substantial waste reduction. Some such modifications are of a chemical nature. Changes in chemical reaction conditions can minimize production of by-product hazardous substances. In some cases, potentially hazardous catalysts, such as those formulated from toxic substances, can be replaced by catalysts that are nonhazardous or that can be recycled rather than discarded. Wastes can be minimized by volume reduction, for example through dewatering and drying sludge.

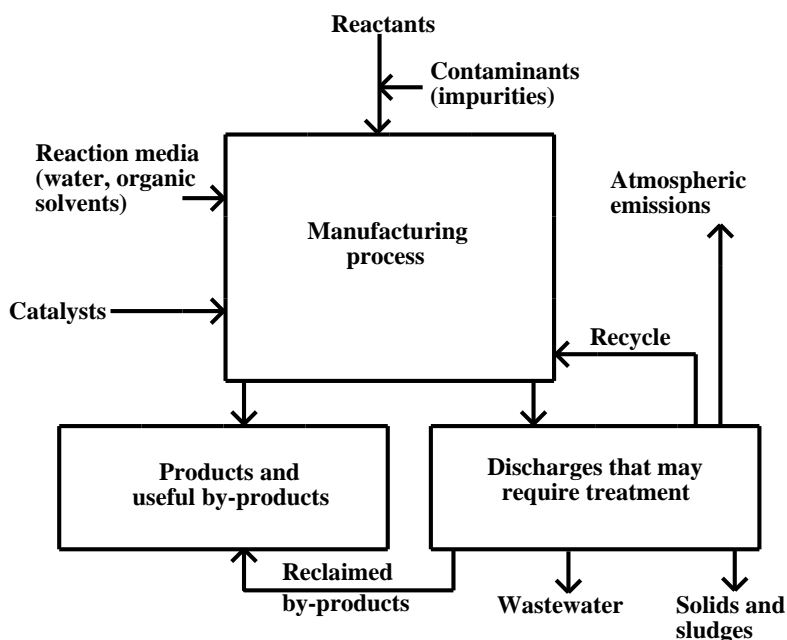


Figure 22.2 Chemical manufacturing process from the viewpoint of discharges and waste minimization.

Many kinds of waste streams are candidates for minimization. As examples, such waste streams identified at U.S. Government federal facilities have included solvents used for cleaning and degreasing, spent motor oil from gasoline and diesel engines, leftover and waste paint thinners, antifreeze/antiboil engine cooling formulations, batteries, inks, exposed photographic film, and pathology wastes.<sup>3</sup> The sources of the wastes are as varied as the waste streams themselves. Motor pool maintenance garages generate used motor oil and spent coolants. Hospitals, clinics, and medical laboratories generate pathology wastes. Aircraft maintenance depots where aircraft are cleaned, chemically stripped of paint and coatings, repainted, and electroplated generate large quantities of effluents, including organic materials.<sup>4</sup> Other facilities generating wastes include equipment- and arms-maintenance facilities, photo developing and printing laboratories, paint shops, and arts and crafts shops.

A crucial part of the process for reducing and minimizing wastes is the development of a material balance, which is an integral part of the practice of industrial ecology.<sup>5</sup> Such a balance addresses various aspects of waste streams, including sources, identification, and quantities of wastes and methods and costs of handling,

treatment, recycling, and disposal. Priority waste streams can then be subjected to detailed process investigations to obtain the information needed to reduce wastes.

There are encouraging signs of progress in the area of waste minimization. All major companies have initiated programs to minimize quantities of wastes produced. A typical success story is a 97% reduction of landfill wastes from Mobil's Torrance petroleum refinery from 1989 to 1993. During the same period, the refinery went from less than 1% waste recycle to more than 70%. One of the technologies used for waste reduction was the Mobil Oil Sludge Coking Process.<sup>6</sup> Similar success stories in reducing wastes can be cited by a number of concerns in the U.S. and throughout the world.

## 22.3 RECYCLING

Wherever possible, recycling and reuse should be accomplished on-site because it avoids having to move wastes, and because a process that produces recyclable materials is often the most likely to have use for them. The four broad areas in which something of value can be obtained from wastes are the following:

- Direct recycle as raw material to the generator, as with the return to feedstock of raw materials not completely consumed in a synthesis process
- Transfer as a raw material to another process; a substance that is a waste product from one process may serve as a raw material for another, sometimes in an entirely different industry
- Utilization for pollution control or waste treatment, such as use of waste alkali to neutralize waste acid
- Recovery of energy, for example, from the incineration of combustible hazardous wastes

### Examples of Recycling

Recycling of scrap industrial impurities and products occurs on a large scale with a number of different materials. Most of these materials are not hazardous but, as with most large-scale industrial operations, their recycling may involve the use or production of hazardous substances. Some of the more important examples are the following:

- **Ferrous metals** composed primarily of iron and used largely as feedstock for electric-arc furnaces
- **Nonferrous metals**, including aluminum (which ranks next to iron in terms of quantities recycled), copper and copper alloys, zinc, lead, cadmium, tin, silver, and mercury
- **Metal compounds**, such as metal salts
- **Inorganic substances** including alkaline compounds (such as sodium hydroxide used to remove sulfur compounds from petroleum products),

acids (steel pickling liquor where impurities permit reuse), and salts (for example, ammonium sulfate from coal coking used as fertilizer)

- **Glass**, which makes up about 10 % of municipal refuse
- **Paper**, commonly recycled from municipal refuse
- **Plastic**, consisting of a variety of moldable polymeric materials and composing a major constituent of municipal wastes
- **Rubber**
- **Organic substances**, especially solvents and oils, such as hydraulic and lubricating oils
- **Catalysts** from chemical synthesis or petroleum processing
- Materials with **agricultural uses**, such as waste lime or phosphate-containing sludges used to treat and fertilize acidic soils

## Waste Oil Utilization and Recovery

**Waste oil** generated from lubricants and hydraulic fluids is one of the more commonly recycled materials. Annual production of waste oil in the U.S. is of the order of 4 billion liters. Around half of this amount is burned as fuel and lesser quantities are recycled or disposed of as waste. The collection, recycling, treatment, and disposal of waste oil are all complicated by the fact that it comes from diverse, widely dispersed sources and contains several classes of potentially hazardous contaminants. These are divided between organic constituents (polycyclic aromatic hydrocarbons, chlorinated hydrocarbons) and inorganic constituents (aluminum, chromium, and iron from wear of metal parts; barium and zinc from oil additives; lead from leaded gasoline).

### *Recycling Waste Oil*

The processes used to convert waste oil to a feedstock hydrocarbon liquid for lubricant formulation are illustrated in [Figure 22.3](#). The first of these uses distillation to remove water and light ends that have come from condensation and contaminant fuel. The second, or processing, step may be a vacuum distillation in which the three

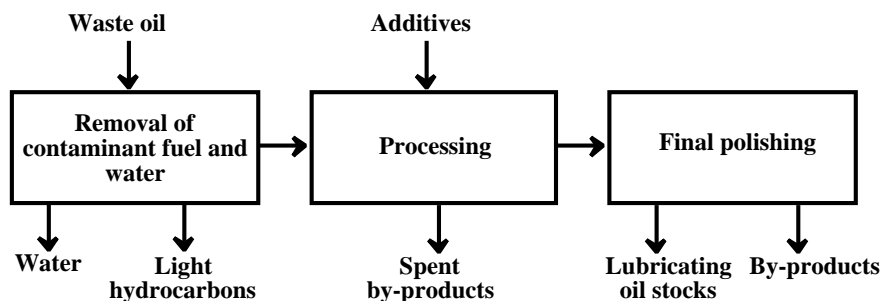


Figure 22.3 Major steps in reprocessing waste oil.

products are oil for further processing, a fuel oil cut, and a heavy residue. The processing step may also employ treatment with a mixture of solvents including isopropyl and butyl alcohols and methylethyl ketone to dissolve the oil and leave contaminants as a sludge; or contact with sulfuric acid to remove inorganic contaminants followed by treatment with clay to take out acid and contaminants that cause odor and color. The third step shown in [Figure 22.3](#) employs vacuum distillation to separate lubricating oil stocks from a fuel fraction and heavy residue. This phase of treatment may also involve hydrofinishing, treatment with clay, and filtration.

### *Waste Oil Fuel*

For economic reasons, waste oil that is to be used for fuel is given minimal treatment of a physical nature, including settling, removal of water, and filtration. Metals in waste fuel oil become highly concentrated in its fly ash, which may be hazardous.

### **Waste Solvent Recovery and Recycle**

The recovery and recycling of waste solvents has some similarities to the recycling of waste oil and is also an important enterprise. Among the many solvents listed as hazardous wastes and recoverable from wastes are dichloromethane, tetrachloroethylene, trichloroethylene, 1,1,1-trichloroethane, benzene, liquid alkanes, 2-nitropropane, methylisobutyl ketone, and cyclohexanone. For reasons of both economics and pollution control, many industrial processes that use solvents are equipped for solvent recycle. The basic scheme for solvent reclamation and reuse is shown in [Figure 22.4](#).

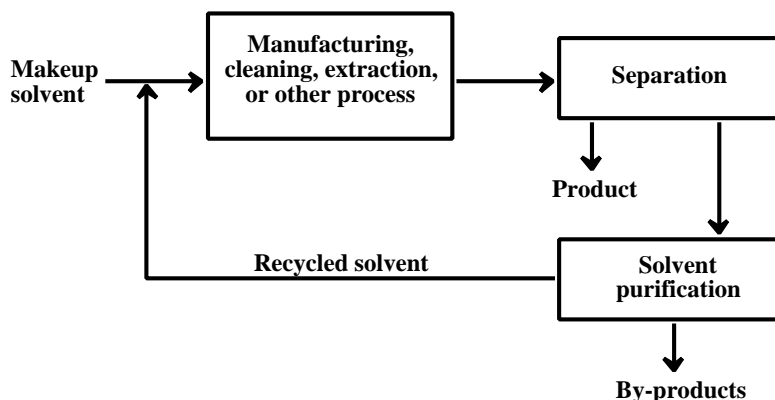


Figure 22.4 Overall process for recycling solvents.

A number of operations are used in solvent purification. Entrained solids are removed by settling, filtration, or centrifugation. Drying agents may be used to remove water from solvents, and various adsorption techniques and chemical treatment may be required to free the solvent from specific impurities. Fractional distillation, often requiring several distillation steps, is the most important operation in solvent purification and recycling. It is used to separate solvents from impurities, water, and other solvents.



## Recovery of Water from Wastewater

It is often desirable to reclaim water from wastewater.<sup>7</sup> This is especially true in regions where water is in short supply. Even where water is abundant, water recycling is desirable to minimize the amount of water that is discharged.

A little more than half of the water used in the U.S. is consumed by agriculture, primarily for irrigation. Steam-generating power plants consume about one-fourth of the water, and other uses, including manufacturing and domestic uses, account for the remainder.

The three major manufacturing consumers of water are chemicals and allied products, paper and allied products, and primary metals. These industries use water for cooling, processing, and boilers. Their potential for water reuse is high and their total consumption of water is projected to drop in future years as recycling becomes more common.

The degree of treatment required for reuse of wastewater depends upon the water's intended use. Water used for industrial quenching and washing usually requires the least treatment, and wastewater from some other processes may be suitable for these purposes without additional treatment. At the other end of the scale, boiler makeup water, potable (drinking) water, water used to directly recharge aquifers, and water that people will directly contact (in boating, water skiing, and similar activities) must be of very high quality.

The treatment processes applied to wastewater for reuse and recycle depend upon both the characteristics of the wastewater and its intended uses. Solids can be removed by sedimentation and filtration. Biochemical oxygen demand is reduced by biological treatment, including trickling filters and activated sludge treatment. For uses conducive to the growth of nuisance algae, nutrients may have to be removed. The easiest of these to handle is nutrient phosphate, which can be precipitated with lime. Nitrogen can be removed by denitrification processes.

Two of the major problems with industrial water recycling are heavy metals and dissolved toxic organic species. Heavy metals may be removed by ion exchange or precipitation by base or sulfide. The organic species are usually removed with activated carbon filtration. Some organic species are biologically degraded by bacteria in biological wastewater treatment.

One of the greater sources of potentially hazardous wastewater arises from oil-water separators at wash racks where manufactured parts and materials are washed. Because of the use of surfactants and solvents in the washwater, the separated water tends to contain emulsified oil that is incompletely separated in an oil-water separator. In addition, the sludge that accumulates at the bottom of the separator may contain hazardous constituents, including heavy metals and some hazardous organic constituents. Several measures that include the incorporation of good industrial ecology practice can be taken to eliminate these problems.<sup>8</sup> One such measure is to eliminate the use of surfactants and solvents that tend to contaminate the water, and to use surfactants and solvents that are more amenable to separation and treatment. Another useful measure is to treat the water to remove harmful constituents and recycle it. This not only conserves water and reduces disposal costs, but also enables recycling of surfactants and other additives.

The ultimate water quality is achieved by processes that remove solutes from water, leaving pure H<sub>2</sub>O. A combination of activated carbon treatment to remove

organics, cation exchange to remove dissolved cations, and anion exchange for dissolved anions can provide very high-quality water from wastewater. Reverse osmosis (see Chapter 8) can accomplish the same objective. However, these processes generate spent activated carbon, ion exchange resins that require regeneration, and concentrated brines (from reverse osmosis) that require disposal, all of which have the potential to end up as hazardous wastes.

## 22.4 PHYSICAL METHODS OF WASTE TREATMENT

This section addresses predominantly physical methods for waste treatment and the following section addresses methods that utilize chemical processes. It should be kept in mind that most waste treatment measures have both physical and chemical aspects. The appropriate treatment technology for hazardous wastes obviously depends upon the nature of the wastes. These may consist of volatile wastes (gases, volatile solutes in water, gases or volatile liquids held by solids, such as catalysts), liquid wastes (wastewater, organic solvents), dissolved or soluble wastes (water-soluble inorganic species, water-soluble organic species, compounds soluble in organic solvents), semisolids (sludges, greases), and solids (dry solids, including granular solids with a significant water content, such as dewatered sludges, as well as solids suspended in liquids). The type of physical treatment to be applied to wastes depends strongly upon the physical properties of the material treated, including state of matter, solubility in water and organic solvents, density, volatility, boiling point, and melting point.

As shown in [Figure 22.5](#), waste treatment may occur at three major levels—**primary**, **secondary**, and **polishing**—somewhat analogous to the treatment of wastewater (see Chapter 8). Primary treatment is generally regarded as preparation for further treatment, although it can result in the removal of byproducts and reduction of the quantity and hazard of the waste. Secondary treatment detoxifies, destroys, and removes hazardous constituents. Polishing usually refers to treatment of water that is removed from wastes so that it can be safely discharged. However, the term can be broadened to apply to the treatment of other products as well so that they can be safely discharged or recycled.

### Methods of Physical Treatment

Knowledge of the physical behavior of wastes has been used to develop various unit operations for waste treatment that are based upon physical properties. These operations include the following:

- Phase separation
  - Filtration
- Phase transition
  - Distillation
  - Evaporation
  - Physical precipitation
- Phase transfer
  - Extraction
  - Sorption
- Membrane separations
  - Reverse osmosis
  - Hyper- and ultrafiltration

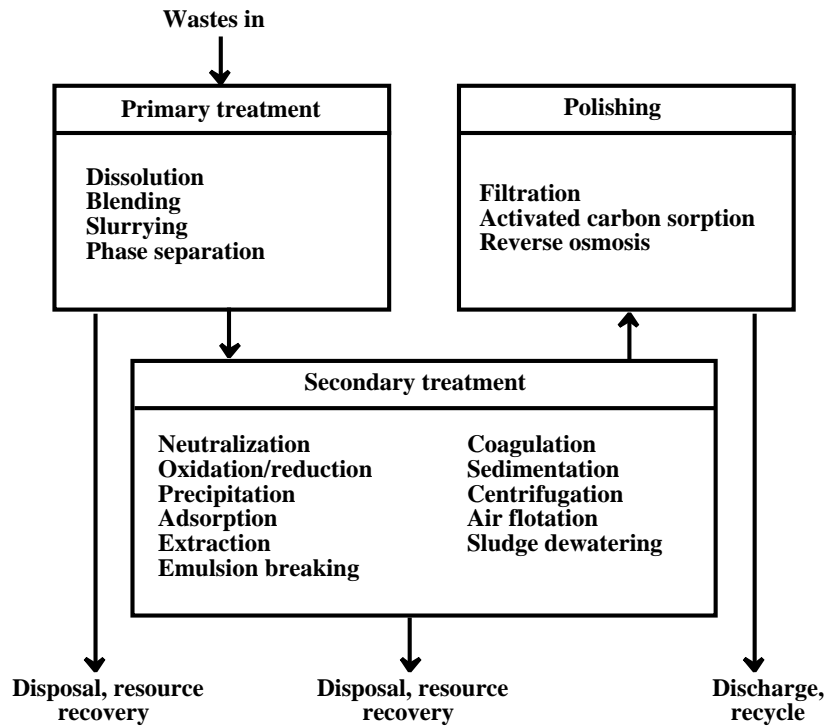


Figure 22.5 Major phases of waste treatment.

### *Phase Separations*

The most straightforward means of physical treatment involves separation of components of a mixture that are already in two different phases. **Sedimentation** and **decanting** are easily accomplished with simple equipment. In many cases the separation must be aided by mechanical means, particularly **filtration** or **centrifugation**. **Flotation** is used to bring suspended organic matter or finely divided particles to the surface of a suspension. In the process of **dissolved air flotation** (DAF), air is dissolved in the suspending medium under pressure and comes out of solution when the pressure is released as minute air bubbles attached to suspended particles, which causes the particles to float to the surface.

An important and often difficult waste-treatment step is **emulsion breaking**, in which colloidal-sized **emulsions** are caused to aggregate and settle from suspension. Agitation, heat, acid, and the addition of **coagulants** consisting of organic polyelectrolytes, or inorganic substances such as an aluminum salt, can be used for this purpose. The chemical additive acts as a flocculating agent to cause the particles to stick together and settle out.

### *Phase Transition*

A second major class of physical separation is that of **phase transition** in which a material changes from one physical phase to another. It is best exemplified by

**distillation**, which is used in treating and recycling solvents, waste oil, aqueous phenolic wastes, xylene contaminated with paraffin from histological laboratories, and mixtures of ethylbenzene and styrene. Distillation produces **distillation bottoms** (still bottoms), which are often hazardous and polluting. These consist of unevaporated solids, semisolid tars, and sludges from distillation. Specific examples with their hazardous-waste numbers are distillation bottoms from the production of acetaldehyde from ethylene (hazardous-waste number K009), and still bottoms from toluene reclamation distillation in the production of disulfoton (K036). The landfill disposal of these and other hazardous distillation bottoms used to be widely practiced but is now severely limited.

**Evaporation** is usually employed to remove water from an aqueous waste to concentrate it. A special case of this technique is **thin-film evaporation** in which volatile constituents are removed by heating a thin layer of liquid or sludge waste spread on a heated surface.

**Drying**—removal of solvent or water from a solid or semisolid (sludge) or the removal of solvent from a liquid or suspension—is a very important operation because water is often the major constituent of waste products, such as sludges obtained from emulsion breaking. In **freeze drying**, the solvent, usually water, is sublimed from a frozen material. Hazardous-waste solids and sludges are dried to reduce the quantity of waste, to remove solvent or water that might interfere with subsequent treatment processes, and to remove hazardous volatile constituents. Dewatering can often be improved with addition of a filter aid, such as diatomaceous earth, during the filtration step.

**Stripping** is a means of separating volatile components from less volatile ones in a liquid mixture by the partitioning of the more volatile materials to a gas phase of air or steam (steam stripping). The gas phase is introduced into the aqueous solution or suspension containing the waste in a stripping tower that is equipped with trays or packed to provide maximum turbulence and contact between the liquid and gas phases. The two major products are condensed vapor and a stripped bottoms residue. Examples of two volatile components that can be removed from water by air stripping are benzene and dichloromethane. Air stripping can also be used to remove ammonia from water that has been treated with a base to convert ammonium ion to volatile ammonia.

**Physical precipitation** is used here as a term to describe processes in which a solid forms from a solute in solution as a result of a physical change in the solution, as compared with chemical precipitation (see Section 22.5), in which a chemical reaction in solution produces an insoluble material. The major changes that can cause physical precipitation are cooling the solution, evaporation of solvent, or alteration of solvent composition. The most common type of physical precipitation by alteration of solvent composition occurs when a water-miscible organic solvent is added to an aqueous solution so that the solubility of a salt is lowered below its concentration in the solution.

### *Phase Transfer*

**Phase transfer** consists of the transfer of a solute in a mixture from one phase to another. An important type of phase transfer process is **solvent extraction**, a process

in which a substance is transferred from solution in one solvent (usually water) to another (usually an organic solvent) without any chemical change taking place. When solvents are used to leach substances from solids or sludges, the process is called **leaching**. Solvent extraction and the major terms applicable to it are summarized in Figure 22.6. The same terms and general principles apply to leaching. The major application of solvent extraction to waste treatment has been in the removal of phenol from by-product water produced in coal coking, petroleum refining, and chemical syntheses that involve phenol.

One of the more promising approaches to solvent extraction and leaching of hazardous wastes is the use of **supercritical fluids**, most commonly CO<sub>2</sub>, as extraction solvents. As discussed in Chapter 20, Section 20.7, a supercritical fluid is a substance above its critical temperature and pressure (31.1°C and 73.8 atm, respectively, for CO<sub>2</sub>) with characteristics of both liquid and gas. After a substance has been extracted from a waste into a supercritical fluid, the pressure can be released, resulting in separation of the substance extracted. The fluid can then be compressed again and recirculated through the extraction system. Some possibilities for treatment of hazardous wastes by extraction with supercritical CO<sub>2</sub> include removal of organic contaminants from wastewater, extraction of organohalide pesticides from soil, extraction of oil from emulsions used in aluminum and steel processing, and regeneration of spent activated carbon. Waste oils contaminated with PCBs, metals, and water can be purified using supercritical ethane.

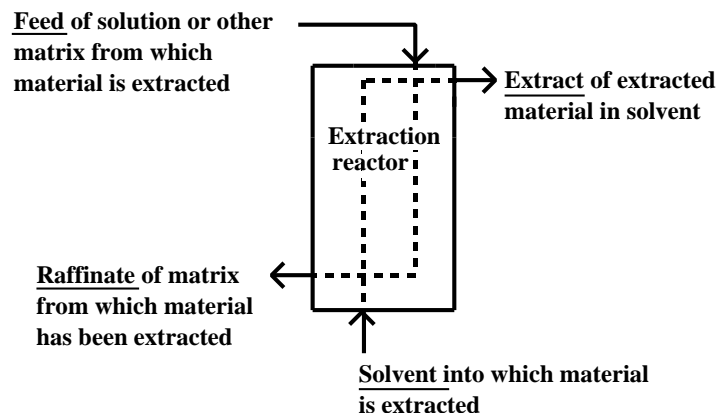


Figure 22.6 Outline of solvent extraction/leaching process with important terms underlined.

Transfer of a substance from a solution to a solid phase is called **sorption**. The most important sorbent is **activated carbon** used for several purposes in waste treatment; in some cases it is adequate for complete treatment. It can also be applied to pretreatment of waste streams going into processes such as reverse osmosis to improve treatment efficiency and reduce fouling. Effluents from other treatment processes, such as biological treatment of degradable organic solutes in water, can be polished with activated carbon. Activated carbon sorption is most effective for removing from water those hazardous-waste materials that are poorly water-soluble and that have high molar masses, such as xylene, naphthalene (U165), cyclohexane (U056); chlorinated hydrocarbons, phenol (U188), aniline (U012), dyes, and surfac-

tants. Activated carbon does not work well for organic compounds that are highly water-soluble or polar.

Solids other than activated carbon can be used for sorption of contaminants from liquid wastes. These include synthetic resins composed of organic polymers and mineral substances. Of the latter, clay is employed to remove impurities from waste lubricating oils in some oil recycling processes.

### *Molecular Separation*

A third major class of physical separation is **molecular separation**, often based upon **membrane processes** in which dissolved contaminants or solvent pass through a size-selective membrane under pressure. The products are a relatively pure solvent phase (usually water) and a concentrate enriched in the solute impurities. **Hyperfiltration** allows passage of species with molecular masses of about 100 to 500, whereas **ultrafiltration** is used for the separation of organic solutes with molar masses of 500 to 1,000,000. With both of these techniques, water and lower molar mass solutes under pressure pass through the membrane as a stream of purified **permeate**, leaving behind a stream of **concentrate** containing impurities in solution or suspension. Ultrafiltration and hyperfiltration are especially useful for concentrating suspended oil, grease, and fine solids in water. They also serve to concentrate solutions of large organic molecules and heavy metal ion complexes.

**Reverse osmosis** is the most widely used of the membrane techniques. Although superficially similar to ultrafiltration and hyperfiltration, it operates on a different principle in that the membrane is selectively permeable to water and excludes ionic solutes. Reverse osmosis uses high pressures to force permeate through the membrane, producing a concentrate containing high levels of dissolved salts.

**Electrodialysis**, sometimes used to concentrate plating wastes, employs membranes alternately permeable to cations and to anions. The driving force for the separation is provided by electrolysis with a direct current between two electrodes. Alternate layers between the membranes contain concentrate (brine) and purified water.

## **22.5 CHEMICAL TREATMENT: AN OVERVIEW**

The applicability of chemical treatment to wastes depends upon the chemical properties of the waste constituents, particularly acid-base, oxidation-reduction, precipitation, and complexation behavior; reactivity; flammability/combustibility; corrosivity; and compatibility with other wastes. The chemical behavior of wastes translates to various unit operations for waste treatment that are based upon chemical properties and reactions. These include the following:

- Acid-base neutralization
- Chemical extraction and leaching
- Ion exchange
- Chemical precipitation
- Oxidation
- Reduction

Some of the more sophisticated means available for treatment of wastes have been developed for pesticide disposal.

## Acid-Base Neutralization

Waste acids and bases are treated by **neutralization**:

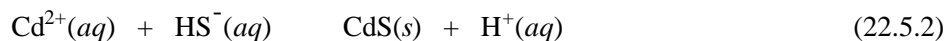


Although simple in principle, neutralization can present some problems in practice. These include evolution of volatile contaminants, mobilization of soluble substances, excessive heat generated by the neutralization reaction, and corrosion to apparatus. By adding too much or too little of the neutralizing agent, it is possible to get a product that is too acidic or basic. Lime,  $\text{Ca}(\text{OH})_2$ , is widely used as a base for treating acidic wastes. Because of lime's limited solubility, solutions of excess lime do not reach extremely high pH values. Sulfuric acid,  $\text{H}_2\text{SO}_4$ , is a relatively inexpensive acid for treating alkaline wastes. However, addition of too much sulfuric acid can produce highly acidic products; for some applications, acetic acid  $\text{CH}_3\text{COOH}$ , is preferable. As noted above, acetic acid is a weak acid and an excess of it does little harm. It is also a natural product and biodegradable.

Neutralization, or pH adjustment, is often required prior to the application of other waste treatment processes. Processes that may require neutralization include oxidation-reduction, activated carbon sorption, wet air oxidation, stripping, and ion exchange. Microorganisms usually require a pH in the range of 6–9, so neutralization may be required prior to biochemical treatment.

## Chemical Precipitation

**Chemical precipitation** is used in hazardous-waste treatment primarily for the removal of heavy-metal ions from water as shown below for the chemical precipitation of cadmium:

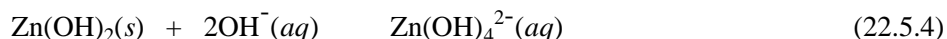


### *Precipitation of Metals*

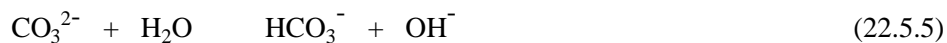
The most widely used means of precipitating metal ions is by the formation of hydroxides such as chromium(III) hydroxide:



The source of hydroxide ion is a base (alkali), such as lime ( $\text{Ca}(\text{OH})_2$ ), sodium hydroxide ( $\text{NaOH}$ ), or sodium carbonate ( $\text{Na}_2\text{CO}_3$ ). Most metal ions tend to produce basic salt precipitates, such as basic copper(II) sulfate,  $\text{CuSO}_4 \cdot 3\text{Cu}(\text{OH})_2$ , which is formed as a solid when hydroxide is added to a solution containing  $\text{Cu}^{2+}$  and  $\text{SO}_4^{2-}$  ions. The solubilities of many heavy metal hydroxides reach a minimum value, often at a pH in the range of 9–11, then increase with increasing pH values due to the formation of soluble hydroxo complexes, as illustrated by the following reaction:

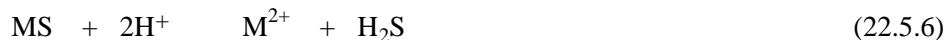


The chemical precipitation method that is used most is precipitation of metals as hydroxides and basic salts with lime. Sodium carbonate can be used to precipitate metal hydroxides ( $\text{Fe}(\text{OH})_3 \cdot x\text{H}_2\text{O}$ ) carbonates ( $\text{CdCO}_3$ ), or basic carbonate salts ( $2\text{PbCO}_3 \cdot \text{Pb}(\text{OH})_2$ ). The carbonate anion produces hydroxide by virtue of its hydrolysis reaction with water:

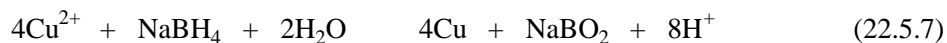


Carbonate, alone, does not give as high a pH as do alkali metal hydroxides, which may have to be used to precipitate metals that form hydroxides only at relatively high pH values.

The solubilities of some heavy metal sulfides are extremely low, so precipitation by  $\text{H}_2\text{S}$  or other sulfides (see Reaction 22.5.2) can be a very effective means of treatment. Hydrogen sulfide is a toxic gas that is itself considered to be a hazardous waste (U135). Iron(II) sulfide (ferrous sulfide) can be used as a safe source of sulfide ion to produce sulfide precipitates with other metals that are less soluble than  $\text{FeS}$ . However, toxic  $\text{H}_2\text{S}$  can be produced when metal sulfide wastes contact acid:



Some metals can be precipitated from solution in the elemental metal form by the action of a reducing agent such as sodium borohydride,



or with more active metals in a process called **cementation**:



Regardless of the method used to precipitate a metal, the form of the metal in the waste solution can be an important consideration. Chelated metals can be especially difficult to remove. For example, difficulties encountered in precipitating copper from waste printed circuit board formulations revealed that chelation of the copper by EDTA chelant was responsible for the problem.<sup>9</sup>

### *Coprecipitation of Metals*

In some cases, advantage may be taken of the phenomenon of coprecipitation to remove metals from wastes. A good example of this application is the coprecipitation of lead from battery industry wastewater with iron(III) hydroxide. Raising the pH of such a wastewater consisting of dilute sulfuric acid and contaminated with  $\text{Pb}^{2+}$  ion precipitates lead as several species, including  $\text{PbSO}_4$ ,  $\text{Pb}(\text{OH})_2$ , and  $\text{Pb}(\text{OH})_2 \cdot 2\text{PbCO}_3$ . In the presence of iron(III), gelatinous  $\text{Fe}(\text{OH})_3$  forms, which coprecipitates the lead, leading to much lower values of lead concentration than would otherwise be possible. Effective removal of lead from battery industry wastewater to below 0.2 ppm has been achieved by first adding an optimum quantity of iron(III), adjustment of the pH to a range of 9–9.5, addition of a polyelectrolyte to aid coagulation, and filtration.<sup>10</sup>



## Oxidation/Reduction

As shown by the reactions in Table 22.1, **oxidation** and **reduction** can be used for the treatment and removal of a variety of inorganic and organic wastes. Some waste oxidants can be used to treat oxidizable wastes in water and cyanides. Ozone, O<sub>3</sub>, is a strong oxidant that can be generated on-site by an electrical discharge through dry air or oxygen. Ozone employed as an oxidant gas at levels of 1–2 wt% in air and 2–5 wt% in oxygen has been used to treat a large variety of oxidizable contaminants, effluents, and wastes including wastewater and sludges containing oxidizable constituents.

**Table 22.1 Oxidation-Reduction Reactions Used to Treat Wastes**

Waste Substance	Reaction with Oxidant or Reductant	
<i>Oxidation of Organics</i>		
Organic matter {CH <sub>2</sub> O}	{CH <sub>2</sub> O} + 2{O}	CO <sub>2</sub> + H <sub>2</sub> O
Aldehyde	CH <sub>3</sub> CHO + {O}	CH <sub>3</sub> COOH (acid)
<i>Oxidation of Inorganics</i>		
Cyanide	2CN <sup>-</sup> + 5OCl <sup>-</sup> + H <sub>2</sub> O	N <sub>2</sub> + 2HCO <sub>3</sub> <sup>-</sup> + 5Cl <sup>-</sup>
Iron(II)	4Fe <sup>2+</sup> + O <sub>2</sub> + 10H <sub>2</sub> O	4Fe(OH) <sub>3</sub> + 8H <sup>+</sup>
Sulfur dioxide	2SO <sub>2</sub> + O <sub>2</sub> + 2H <sub>2</sub> O	2H <sub>2</sub> SO <sub>4</sub>
<i>Reduction of Inorganics</i>		
Chromate	2CrO <sub>4</sub> <sup>2-</sup> + 3SO <sub>2</sub> + 4H <sup>+</sup>	Cr <sub>2</sub> (SO <sub>4</sub> ) <sub>3</sub> + 2H <sub>2</sub> O
Permanganate	MnO <sub>4</sub> <sup>-</sup> + 3Fe <sup>2+</sup> + 7H <sub>2</sub> O	MnO <sub>2</sub> (s) + 3Fe(OH) <sub>3</sub> (s) + 5H <sup>+</sup>

## Electrolysis

As shown in Figure 22.7, **electrolysis** is a process in which one species in solution (usually a metal ion) is reduced by electrons at the **cathode** and another gives up electrons to the **anode** and is oxidized there. In hazardous-waste applications, electrolysis is most widely used in the recovery of cadmium, copper, gold, lead, silver, and zinc. Metal recovery by electrolysis is made more difficult by the presence of cyanide ion, which stabilizes metals in solution as the cyanide complexes, such as Ni(CN)<sub>4</sub><sup>2-</sup>.

Electrolytic removal of contaminants from solution can be by direct electro-deposition, particularly of reduced metals, and as the result of secondary reactions of

electrolytically generated precipitating agents. A specific example of both is the electrolytic removal of both cadmium and nickel from wastewater contaminated by nickel/cadmium battery manufacture using fibrous carbon electrodes.<sup>11</sup> At the cathode, cadmium is removed directly by reduction to the metal:

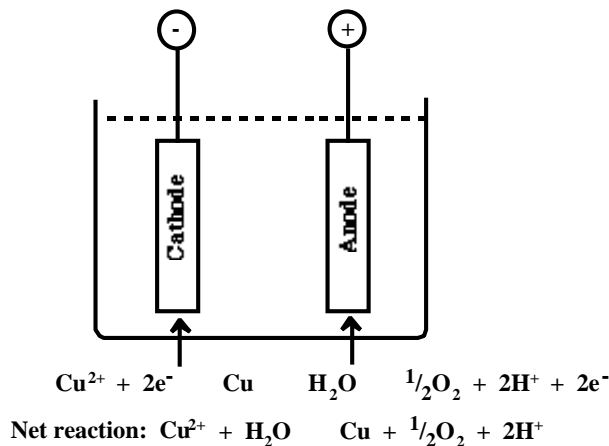
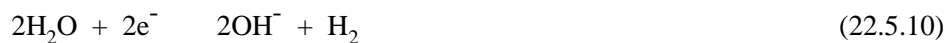


Figure 22.7 Electrolysis of copper solution.

At relatively high cathodic potentials, hydroxide is formed by the electrolytic reduction of water,



or by the reduction of molecular oxygen, if it is present:



If the localized pH at the cathode surface becomes sufficiently high, cadmium can be precipitated and removed as colloidal  $\text{Cd}(\text{OH})_2$ . The direct electrodeposition of nickel is too slow to be significant, but it is precipitated as solid  $\text{Ni}(\text{OH})_2$  at pH values above 7.5.

Cyanide, which is often present as an ingredient of electroplating baths with metals such as cadmium and nickel, can be removed by oxidation with electrolytically generated elemental chlorine at the anode. Chlorine is generated by the anodic oxidation of added chloride ion:



The electrolytically generated chlorine then breaks down cyanide by a series of reactions for which the overall reaction is the following:



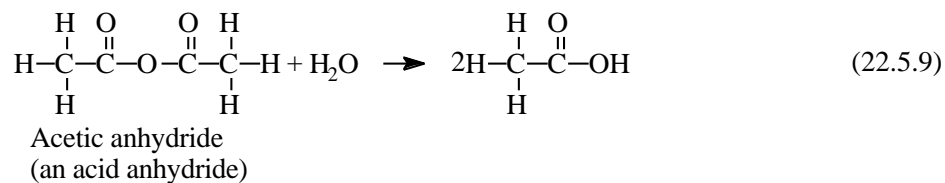
## Hydrolysis

One of the ways to dispose of chemicals that are reactive with water is to allow them to react with water under controlled conditions, a process called **hydrolysis**. Inorganic chemicals that can be treated by hydrolysis include metals that react with water; metal carbides, hydrides, amides, alkoxides, and halides; and nonmetal oxyhalides and sulfides. Examples of the treatment of these classes of inorganic species are given in [Table 22.2](#).

**Table 22.2 Inorganic Chemicals That Can Be Treated by Hydrolysis**

Class of chemical	Reaction with oxidant or reductant
Active metals (calcium)	$\text{Ca} + 2\text{H}_2\text{O} \rightarrow \text{H}_2 + \text{Ca(OH)}_2$
Hydrides (sodium aluminum hydride)	$\text{NaAlH}_4 + 4\text{H}_2\text{O} \rightarrow 4\text{H}_2 + \text{NaOH} + \text{Al(OH)}_3$
Carbides (calcium carbide)	$\text{CaC}_2 + 2\text{H}_2\text{O} \rightarrow \text{Ca(OH)}_2 + \text{C}_2\text{H}_2$
Amides (sodium amide)	$\text{NaNH}_2 + \text{H}_2\text{O} \rightarrow \text{NaOH} + \text{NH}_3$
Halides (silicon tetrachloride)	$\text{SiCl}_4 + 2\text{H}_2\text{O} \rightarrow \text{SiO}_2 + 4\text{HCl}$
Alkoxides (sodium ethoxide)	$\text{NaOC}_2\text{H}_5 + \text{H}_2\text{O} \rightarrow \text{NaOH} + \text{C}_2\text{H}_5\text{OH}$

Organic chemicals can also be treated by hydrolysis. For example, toxic acetic anhydride is hydrolyzed to relatively safe acetic acid:



## Chemical Extraction and Leaching

**Chemical extraction or leaching** in hazardous-waste treatment is the removal of a hazardous constituent by chemical reaction with an extractant in solution. Poorly soluble heavy metal salts can be extracted by reaction of the salt anions with  $\text{H}^+$  as illustrated by the following:



Acids also dissolve basic organic compounds such as amines and aniline. Extraction with acids should be avoided if cyanides or sulfides are present to prevent formation

of toxic hydrogen cyanide or hydrogen sulfide. Nontoxic weak acids are usually the safest to use. These include acetic acid,  $\text{CH}_3\text{COOH}$ , and the acid salt,  $\text{NaH}_2\text{PO}_4$ .

Chelating agents, such as dissolved ethylenediaminetetraacetate (EDTA,  $\text{HY}^{3-}$ ), dissolve insoluble metal salts by forming soluble species with metal ions:



Heavy-metal ions in soil contaminated by hazardous wastes may be present in a coprecipitated form with insoluble iron(III) and manganese(IV) oxides,  $\text{Fe}_2\text{O}_3$  and  $\text{MnO}_2$ , respectively. These oxides can be dissolved by reducing agents, such as solutions of sodium dithionate/citrate or hydroxylamine. This results in the production of soluble  $\text{Fe}^{2+}$  and  $\text{Mn}^{2+}$  and the release of heavy-metal ions, such as  $\text{Cd}^{2+}$  or  $\text{Ni}^{2+}$ , which are removed with the water.

## Ion Exchange

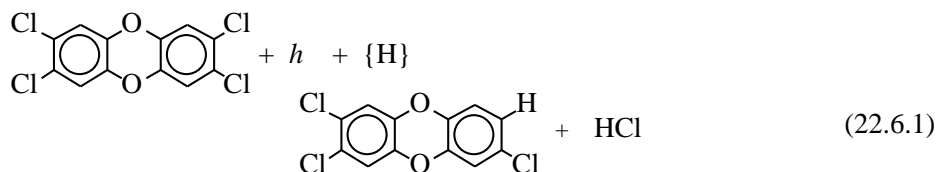
**Ion exchange** is a means of removing cations or anions from solution onto a solid resin, which can be regenerated by treatment with acids, bases, or salts. The greatest use of ion exchange in hazardous-waste treatment is for the removal of low levels of heavy-metal ions from wastewater:



Ion exchange is used in the metal plating industry to purify rinsewater and spent plating bath solutions. Cation exchangers remove cationic metal species, such as  $\text{Cu}^{2+}$ , from such solutions. Anion exchangers remove anionic cyanide metal complexes such as  $\text{Ni}(\text{CN})_4^{2-}$  and chromium(VI) species, such as  $\text{CrO}_4^{2-}$ . Radionuclides can be removed from radioactive and mixed waste by ion exchange resins.

## 22.6 PHOTOLYTIC REACTIONS

**Photolytic** (photochemical) **reactions** were discussed in Chapter 9 and as ideal “green chemistry” reagents in Chapter 20, Section 20.9. *Photolysis* can be used to destroy a number of kinds of hazardous wastes. In such applications it is most useful in breaking chemical bonds in refractory organic compounds. TCDD (see Section 7.10), one of the most troublesome and refractory of wastes, can be treated by ultraviolet radiation in the presence of hydrogen atom donors {H} resulting in reactions such as the following:



As photolysis proceeds, the H–C bonds are broken, the C–O bonds are broken, and the final product is a harmless organic polymer.

An initial photolysis reaction can result in the generation of reactive intermediates that participate in **chain reactions** that lead to the destruction of a

compound. One of the most important reactive intermediates is free radical HO•. In some cases, **sensitizers** are added to the reaction mixture to absorb radiation and generate reactive species that destroy wastes.

Hazardous-waste substances other than TCDD that have been destroyed by photolysis are herbicides (atrazine), 2,4,6-trinitrotoluene (TNT), and polychlorinated biphenyls (PCBs). The addition of a chemical oxidant, such as potassium peroxydisulfate, K<sub>2</sub>S<sub>2</sub>O<sub>8</sub>, enhances destruction by oxidizing active photolytic products.

## 22.7 THERMAL TREATMENT METHODS

Thermal treatment of hazardous wastes can be used to accomplish most of the common objectives of waste treatment—volume reduction; removal of volatile, combustible, mobile organic matter; and destruction of toxic and pathogenic materials. The most widely applied means of thermal treatment of hazardous wastes is **incineration**. Incineration utilizes high temperatures, an oxidizing atmosphere, and often turbulent combustion conditions to destroy wastes. Methods other than incineration that make use of high temperatures to destroy or neutralize hazardous wastes are discussed briefly at the end of this section.

### Incineration

Hazardous-waste incineration will be defined here as a process that involves exposure of the waste materials to oxidizing conditions at a high temperature, usually in excess of 900°C. Normally, the heat required for incineration comes from the oxidation of organically bound carbon and hydrogen contained in the waste material or in supplemental fuel:



These reactions destroy organic matter and generate heat required for endothermic reactions, such as the breaking of C–Cl bonds in organochlorine compounds.

### *Incinerable Wastes*

Ideally, incinerable wastes are predominantly organic materials that will burn with a heating value of at least 5000 Btu/lb and preferably over 8000 Btu/lb. Such heating values are readily attained with wastes having high contents of the most commonly incinerated waste organic substances, including methanol, acetonitrile, toluene, ethanol, amyl acetate, acetone, xylene, methyl ethyl ketone, adipic acid, and ethyl acetate. In some cases, however, it is desirable to incinerate wastes that will not burn alone and that require **supplemental fuel**, such as methane and petroleum liquids. Examples of such wastes are nonflammable organochlorine wastes, some aqueous wastes, or soil in which the elimination of a particularly troublesome contaminant is worth the expense and trouble of incinerating it. Inorganic matter, water, and organic hetero element contents of liquid wastes are important in determining their incinerability.

## Hazardous-Waste Fuel

Many industrial wastes, including hazardous wastes, are burned as **hazardous-waste fuel** for energy recovery in industrial furnaces and boilers and in incinerators for nonhazardous wastes, such as sewage sludge incinerators. This process is called **coincineration**, and more combustible wastes are utilized by it than are burned solely for the purpose of waste destruction. In addition to heat recovery from combustible wastes, it is a major advantage to use an existing on-site facility for waste disposal rather than a separate hazardous-waste incinerator.

## Incineration Systems

The four major components of hazardous-waste incineration systems are shown in [Figure 22.8](#).

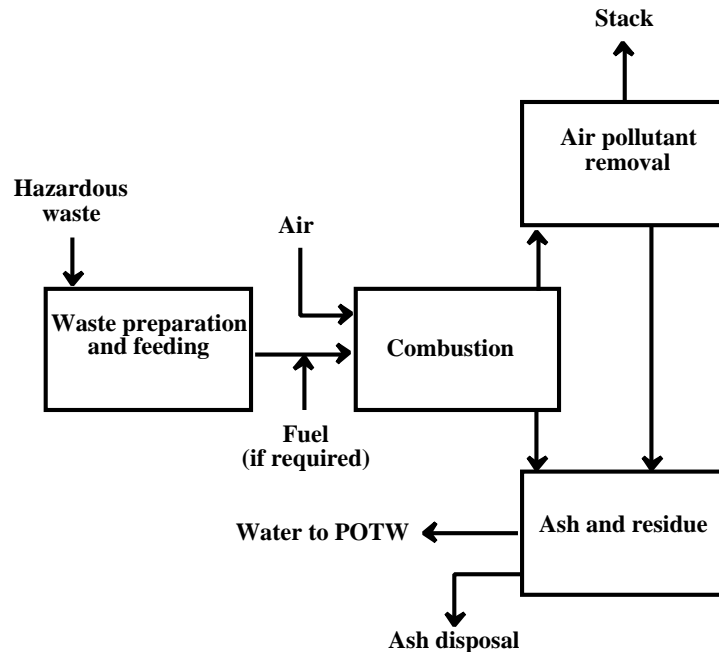


Figure 22.8 Major components of a hazardous-waste incinerator system.

**Waste preparation** for liquid wastes may require filtration, settling to remove solid material and water, blending to obtain the optimum incinerable mixture, or heating to decrease viscosity. Solids may require shredding and screening. Atomization is commonly used to feed liquid wastes. Several mechanical devices, such as rams and augers, are used to introduce solids into the incinerator.

The most common kinds of **combustion chambers** are liquid injection, fixed hearth, rotary kiln, and fluidized bed. These types are discussed in more detail later in this section.

Often the most complex part of a hazardous-waste incineration system is the **air pollution control system**, which involves several operations. The most common operations in air pollution control from hazardous-waste incinerators are combustion

gas cooling, heat recovery, quenching, particulate matter removal, acid gas removal, and treatment and handling of by-product solids, sludges, and liquids.

Hot ash is often quenched in water. Prior to disposal it may require dewatering and chemical stabilization. A major consideration with hazardous-waste incinerators and the types of wastes that are incinerated is the disposal problem posed by the ash, especially with respect to potential leaching of heavy metals.

## Types of Incinerators

hazardous-waste incinerators can be divided among the following, based upon type of combustion chamber:

- **Rotary kiln** (about 40% of U.S. hazardous-waste incinerator capacity) in which the primary combustion chamber is a rotating cylinder lined with refractory materials, and an afterburner downstream from the kiln to complete destruction of the wastes
- **Liquid injection** incinerators (also about 40% of U.S. hazardous-waste incinerator capacity) that burn pumpable liquid wastes dispersed as small droplets
- **Fixed-hearth incinerators** with single or multiple hearths upon which combustion of liquid or solid wastes occurs
- **Fluidized-bed incinerators** in which combustion of wastes is carried out on a bed of granular solid (such as limestone) maintained in a suspended (fluid-like) state by injection of air to remove pollutant acid gas and ash products
- **Advanced design incinerators** including **plasma incinerators** that make use of an extremely hot plasma of ionized air injected through an electrical arc;<sup>12</sup> **electric reactors** that use resistance-heated incinerator walls at around 2200°C to heat and pyrolyze wastes by radiative heat transfer; **infrared systems**, which generate intense infrared radiation by passing electricity through silicon carbide resistance heating elements; **molten salt combustion** that uses a bed of molten sodium carbonate at about 900°C to destroy the wastes and retain gaseous pollutants; and **molten glass processes** that use a pool of molten glass to transfer heat to the waste and to retain products in a poorly leachable glass form

## Combustion Conditions

The key to effective incineration of hazardous wastes lies in the combustion conditions. These require (1) sufficient free oxygen in the combustion zone to ensure combustion of the wastes; (2) turbulence for thorough mixing of waste, oxidant, and (in cases where the waste does not have sufficient fuel content to be burned alone) supplemental fuel; (3) high combustion temperatures above about 900°C to ensure that thermally resistant compounds do react; and (4) sufficient residence time (at least 2 seconds) to allow reactions to occur.

## Effectiveness of Incineration

EPA standards for hazardous-waste incineration are based upon the effectiveness of destruction of the **principal organic hazardous constituents** (POHC). Measurement of these compounds before and after incineration gives the **destruction removal efficiency** (DRE) according to the formula,

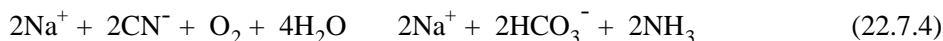
$$\text{DRE} = \frac{W_{\text{in}} - W_{\text{out}}}{W_{\text{in}}} \times 100 \quad (22.7.3)$$

where  $W_{\text{in}}$  and  $W_{\text{out}}$  are the mass flow rates of the principal organic hazardous constituent (POHC) input and output (at the stack downstream from emission controls), respectively. United States EPA regulations call for destruction of 99.99% of POHCs and 99.9999% (“six nines”) destruction of 2,3,7,8-tetrachlorodibenzo-*p*-dioxin, commonly called TCDD or “dioxin.”

## Wet Air Oxidation

Organic compounds and oxidizable inorganic species can be oxidized by oxygen in aqueous solution. The source of oxygen usually is air. Rather extreme conditions of temperature and pressure are required, with a temperature range of 175–327°C and a pressure range of 300–3000 psig (2070–20700 kPa). The high pressures allow a high concentration of oxygen to be dissolved in the water, and the high temperatures enable the reaction to occur.

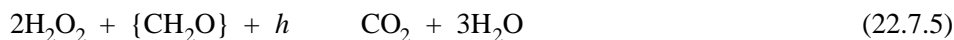
Wet air oxidation has been applied to the destruction of cyanides in electroplating wastewaters. The oxidation reaction for sodium cyanide is the following:



Organic wastes can be oxidized in supercritical water, taking advantage of the ability of supercritical fluids to dissolve organic compounds (see Section 22.4). Wastes are contacted with water and the mixture raised to a temperature and pressure required for supercritical conditions for water. Oxygen is then pumped in sufficient to oxidize the wastes. The process produces only small quantities of CO, and no SO<sub>2</sub> or NO<sub>x</sub>. It can be used to degrade PCBs, dioxins, organochlorine insecticides, benzene, urea, and numerous other materials.

## UV-Enhanced Wet Oxidation

Hydrogen peroxide (H<sub>2</sub>O<sub>2</sub>) can be used as an oxidant in solution assisted by ultraviolet radiation ( $h\nu$ ). For the oxidation of organic species represented in general as {CH<sub>2</sub>O}, the overall reaction is



The ultraviolet radiation breaks chemical bonds and serves to form reactive oxidant species, such as HO•.



## 22.8 BIODEGRADATION OF WASTES

**Biodegradation** of wastes is a term that describes the conversion of wastes by enzymatic biological processes to simple inorganic molecules (mineralization) and, to a certain extent, to biological materials. Usually the products of biodegradation are molecular forms that tend to occur in nature and that are in greater thermodynamic equilibrium with their surroundings than are the starting materials. **Detoxification** refers to the biological conversion of a toxic substance to a less toxic species. Microbial bacteria and fungi possessing enzyme systems required for biodegradation of wastes are usually best obtained from populations of indigenous microorganisms at a hazardous-waste site where the microorganisms have developed the ability to degrade particular kinds of molecules. Biological treatment offers a number of significant advantages and has considerable potential for the degradation of hazardous wastes, even *in situ*.

Under the label of **bioremediation**, the use of microbial processes to destroy hazardous wastes has been the subject of intense investigation in the waste-treatment community for a number of years. Doubts still exist about claims for its effectiveness in a number of applications. It must be kept in mind, however, that there are many factors that can cause biodegradation to fail as a treatment process. Often physical conditions are such that mixing of wastes, nutrients, and electron acceptor species (such as oxygen) is too slow to permit biodegradation to occur at a useful rate. Low temperatures may make reactions too slow to be useful. Toxicants, such as heavy metals, may inhibit biological activity, and some metabolites produced by the microorganisms may be toxic to them.

### Biodegradability

The **biodegradability** of a compound is influenced by its physical characteristics, such as solubility in water and vapor pressure, and by its chemical properties, including molar mass, molecular structure, and presence of various kinds of functional groups, some of which provide a “biochemical handle” for the initiation of biodegradation. With the appropriate organisms and under the right conditions, even substances such as phenol that are considered to be biocidal to most microorganisms can undergo biodegradation.

**Recalcitrant** or **biorefractory** substances are those that resist biodegradation and tend to persist and accumulate in the environment. Such materials are not necessarily toxic to organisms, but simply resist their metabolic attack. However, even some compounds regarded as biorefractory can be degraded by microorganisms that have had the opportunity to adapt to their biodegradation; for example, DDT is degraded by properly acclimated *Pseudomonas*. Chemical pretreatment, especially by partial oxidation, can make some kinds of recalcitrant wastes much more biodegradable.

Properties of hazardous wastes and their media can be changed to increase biodegradability. This can be accomplished by adjustment of conditions to optimum temperature, pH (usually in the range of 6–9), stirring, oxygen level, and material load. Biodegradation can be aided by removal of toxic organic and inorganic substances, such as heavy-metal ions.

## Aerobic Treatment

**Aerobic waste-treatment** processes utilize aerobic bacteria and fungi that require molecular oxygen,  $O_2$ . These processes are often favored by microorganisms, in part because of the high energy yield obtained when molecular oxygen reacts with organic matter. Aerobic waste treatment is well adapted to the use of an activated sludge process. It can be applied to hazardous wastes such as chemical process wastes and landfill leachates. Some systems use powdered activated carbon as an additive to absorb organic wastes that are not biodegraded by microorganisms in the system.

Contaminated soils can be mixed with water and treated in a bioreactor to eliminate biodegradable contaminants in the soil. It is possible, in principle, to treat contaminated soils biologically in place by pumping oxygenated, nutrient-enriched water through the soil in a recirculating system.

## Anaerobic Treatment

**Anaerobic waste treatment** in which microorganisms degrade wastes in the absence of oxygen can be practiced on a variety of organic hazardous wastes. Compared with the aerated activated sludge process, anaerobic digestion requires less energy; yields less sludge by-product; generates hydrogen sulfide ( $H_2S$ ), which precipitates toxic heavy-metal ions; and produces methane gas,  $CH_4$ , which can be used as an energy source.

The overall process for anaerobic digestion is a fermentation process in which organic matter is both oxidized and reduced. The simplified reaction for the anaerobic fermentation of a hypothetical organic substance, “ $\{CH_2O\}$ ”, is the following:

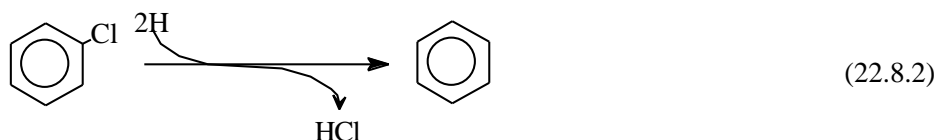


In practice, the microbial processes involved are quite complex. Most of the wastes for which anaerobic digestion is suitable consist of oxygenated compounds, such as acetaldehyde or methylethyl ketone.

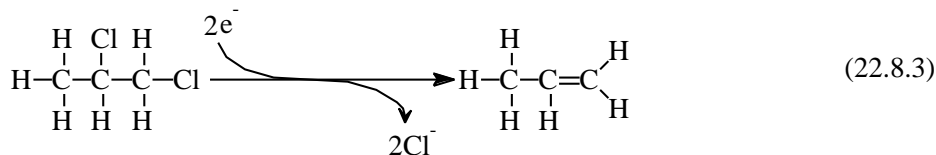
## Reductive Dehalogenation

**Reductive dehalogenation** is a mechanism by which halogen atoms are removed from organohalide compounds by anaerobic bacteria. It is an important means of detoxifying alkyl halides (particularly solvents), aryl halides, and organochlorine pesticides, all of which are important hazardous-waste compounds, and which were discarded in large quantities in some of the older waste disposal dumps. Reductive dehalogenation is the only means by which some of the more highly halogenated waste compounds are biodegraded; such compounds include tetrachloroethene, hexachlorobenzene, pentachlorophenol, and the more highly chlorinated PCB congeners.<sup>13</sup>

The two general processes by which reductive dehalogenation occurs are **hydrogenolysis**, as shown by the example in Equation 22.8.2,



and **vicinal reduction**



Vicinal reduction removes two adjacent halogen atoms, and works only on alkyl halides, not aryl halides. Both processes produce innocuous inorganic halide ( $\text{Cl}^-$ ).

## 22.9 LAND TREATMENT AND COMPOSTING

### Land Treatment

Soil can be viewed as a natural filter for wastes. Soil has physical, chemical, and biological characteristics that can enable waste detoxification, biodegradation, chemical decomposition, and physical and chemical fixation. Therefore, **land treatment** of wastes can be accomplished by mixing the wastes with soil under appropriate conditions.

Soil is a natural medium for a number of living organisms that may have an effect upon biodegradation of hazardous wastes. Of these, the most important are bacteria, including those from the genera *Agrobacterium*, *Arthrobacteri*, *Bacillus*, *Flavobacterium*, and *Pseudomonas*. *Actinomycetes* and fungi are important organisms in decay of vegetable matter and may be involved in biodegradation of wastes.

Microorganisms useful for land treatment of wastes are usually present naturally in sufficient numbers to provide the inoculum required for their growth. The growth of these indigenous microorganisms can be stimulated by adding nutrients and an electron acceptor to act as an oxidant (for aerobic degradation) accompanied by mixing. The most commonly added nutrients are nitrogen and phosphorus. Oxygen can be added by pumping air underground or by treatment with hydrogen peroxide,  $\text{H}_2\text{O}_2$ . In some cases, such as for treatment of hydrocarbons on or near the soil surface, simple tillage provides both oxygen and the mixing required for optimum microbial growth.

Wastes that are amenable to land treatment are biodegradable organic substances. However, in soil contaminated with hazardous wastes, bacterial cultures may develop that are effective in degrading normally recalcitrant compounds through acclimation over a long period of time. Land treatment is most used for petroleum refining wastes and is applicable to the treatment of fuels and wastes from leaking underground storage tanks. It can also be applied to biodegradable organic chemical wastes, including some organohalide compounds. Land treatment is not

suitable for the treatment of wastes containing acids, bases, toxic inorganic compounds, salts, heavy metals, and organic compounds that are excessively soluble, volatile, or flammable.

## **Composting**

**Composting** of hazardous wastes is the biodegradation of solid or solidified materials in a medium other than soil. Bulking material, such as plant residue, paper, municipal refuse, or sawdust can be added to retain water and enable air to penetrate to the waste material. Successful composting of hazardous waste depends upon a number of factors, including those discussed above under land treatment. The first of these is the selection of the appropriate microorganism or **inoculum**. Once a successful composting operation is underway, a good inoculum is maintained by recirculating spent compost to each new batch. Other parameters that must be controlled include oxygen supply, moisture content (which should be maintained at a minimum of about 40%), pH (usually around neutral), and temperature. The composting process generates heat, so, if the mass of the compost pile is sufficiently high, it can be self-heating under most conditions. Some wastes are deficient in nutrients such as nitrogen, which must be supplied from commercial sources or from other wastes.

## **22.10 PREPARATION OF WASTES FOR DISPOSAL**

Immobilization, stabilization, fixation, and solidification are terms that describe sometimes overlapping techniques whereby hazardous wastes are placed in a form suitable for long-term disposal. These aspects of hazardous-waste management are addressed below.

### **Immobilization**

**Immobilization** includes physical and chemical processes that reduce surface areas of wastes to minimize leaching. It isolates the wastes from their environment, especially groundwater, so that they have the least possible tendency to migrate. This is accomplished by physically isolating the waste, reducing its solubility, and decreasing its surface area. Immobilization usually improves the handling and physical characteristics of wastes.

### **Stabilization**

**Stabilization** means the conversion of a waste from its original form to a physically and chemically more stable material that is less likely to cause problems during handling and disposal, and less likely to be mobile after disposal. Stabilization can include chemical reactions that generate products that are less volatile, soluble, and reactive. Solidification, which is discussed below, is one of the most common means of stabilization. Stabilization is required for land disposal of wastes. **Fixation** is a process that binds a hazardous waste in a less mobile and less toxic form; it means much the same thing as stabilization.

## Solidification

**Solidification** may involve chemical reaction of the waste with the solidification agent, mechanical isolation in a protective binding matrix, or a combination of chemical and physical processes. It can be accomplished by evaporation of water from aqueous wastes or sludges, sorption onto solid material, reaction with cement, reaction with silicates, encapsulation, or embedding in polymers or thermoplastic materials.

In many solidification processes, such as reaction with Portland cement, water is an important ingredient of the hydrated solid matrix. Therefore, the solid should not be heated excessively or exposed to extremely dry conditions, which could result in diminished structural integrity from loss of water. In some cases, however, heating a solidified waste is an essential part of the overall solidification procedure. For example, an iron hydroxide matrix can be converted to highly insoluble, refractory iron oxide by heating. Organic constituents of solidified wastes can be converted to inert carbon by heating. Heating is an integral part of the process of vitrification (see below).

### *Sorption to a Solid Matrix Material*

Hazardous-waste liquids, emulsions, sludges, and free liquids in contact with sludges can be solidified and stabilized by fixing onto solid **sorbents**, including activated carbon (for organics), fly ash, kiln dust, clays, vermiculite, and various proprietary materials. Sorption can be done to convert liquids and semisolids to dry solids, improve waste handling, and reduce solubility of waste constituents. Sorption can also be used to improve waste compatibility with substances such as Portland cement used for solidification and setting. Specific sorbents can also be used to stabilize pH and pE (a measure of the tendency of a medium to be oxidizing or reducing, see Chapter 4).

The action of sorbents can include simple mechanical retention of wastes, physical sorption, and chemical reactions. It is important to match the sorbent to the waste. A substance with a strong affinity for water should be employed for wastes containing excess water, and one with a strong affinity for organic materials should be used for wastes with excess organic solvents.

### *Thermoplastics and Organic Polymers*

**Thermoplastics** are solids or semisolids that become liquified at elevated temperatures. Hazardous-waste materials can be mixed with hot thermoplastic liquids and solidified in the cooled thermoplastic matrix, which is rigid but deformable. The thermoplastic material most used for this purpose is asphalt bitumen. Other thermoplastics, such as paraffin and polyethylene, have also been used to immobilize hazardous wastes.

Among the wastes that can be immobilized with thermoplastics are those containing heavy metals, such as electroplating wastes. Organic thermoplastics repel water and reduce the tendency toward leaching in contact with groundwater. Compared with cement, thermoplastics add relatively less material to the waste.

A technique similar to that described above uses **organic polymers** produced in contact with solid wastes to embed the wastes in a polymer matrix. Three kinds of polymers that have been used for this purpose include polybutadiene, urea-formaldehyde, and vinyl ester-styrene polymers. This procedure is more complicated than is the use of thermoplastics but, in favorable cases, yields a product in which the waste is held more strongly.

### *Vitrification*

**Vitrification**, or **glassification**, consists of embedding wastes in a glass material. In this application, glass can be regarded as a high-melting-temperature inorganic thermoplastic. Molten glass can be used, or glass can be synthesized in contact with the waste by mixing and heating with glass constituents—silicon dioxide ( $\text{SiO}_2$ ), sodium carbonate ( $\text{Na}_2\text{CO}_3$ ), and calcium oxide ( $\text{CaO}$ ). Other constituents may include boron oxide,  $\text{B}_2\text{O}_3$ , which yields a borosilicate glass that is especially resistant to changes in temperature and chemical attack. In some cases, glass is used in conjunction with thermal waste destruction processes, serving to immobilize hazardous-waste ash constituents. Some wastes are detrimental to the quality of the glass. Aluminum oxide, for example, may prevent glass from fusing.

Vitrification is relatively complicated and expensive, the latter because of the energy consumed in fusing glass. Despite these disadvantages, it is the favored immobilization technique for some special wastes and has been promoted for solidification of radionuclear wastes because glass is chemically inert and resistant to leaching. However, high levels of radioactivity can cause deterioration of glass and lower its resistance to leaching.

### *Solidification with Cement*

Portland cement is widely used for solidification of hazardous wastes. In this application, Portland cement provides a solid matrix for isolation of the wastes, chemically binds water from sludge wastes, and may react chemically with wastes (for example, the calcium and base in Portland cement react chemically with inorganic arsenic sulfide wastes to reduce their solubilities). However, most wastes are held physically in the rigid Portland cement matrix and are subject to leaching.

As a solidification matrix, Portland cement is most applicable to inorganic sludges containing heavy metal ions that form insoluble hydroxides and carbonates in the basic carbonate medium provided by the cement. The success of solidification with Portland cement strongly depends upon whether the waste adversely affects the strength and stability of the concrete product. A number of substances—organic matter such as petroleum or coal; some silts and clays; sodium salts of arsenate, borate, phosphate, iodate, and sulfide; and salts of copper, lead, magnesium, tin, and zinc—are incompatible with Portland cement because they interfere with its set and cure, producing a mechanically weak product and resulting in deterioration of the cement matrix with time. However, a reasonably good disposal form can be obtained by absorbing organic wastes with a solid material, which in turn is set in Portland cement.

## *Solidification with Silicate Materials*

Water-insoluble **silicates**, (pozzolanic substances) containing oxyanionic silicon such as  $\text{SiO}_3^{2-}$  are used for waste solidification. There are a number of such substances, some of which are waste products, including fly ash, flue dust, clay, calcium silicates, and ground-up slag from blast furnaces. Soluble silicates, such as sodium silicate, may also be used. Silicate solidification usually requires a setting agent, which may be Portland cement (see above), gypsum (hydrated  $\text{CaSO}_4$ ), lime, or compounds of aluminum, magnesium, or iron. The product can vary from a granular material to a concrete-like solid. In some cases, the product is improved by additives, such as emulsifiers, surfactants, activators, calcium chloride, clays, carbon, zeolites, and various proprietary materials.

Success has been reported for the solidification of both inorganic wastes and organic wastes (including oily sludges) with silicates. The advantages and disadvantages of silicate solidification are similar to those of Portland cement discussed above. One consideration that is especially applicable to fly ash is the presence in some silicate materials of leachable hazardous substances, which may include arsenic and selenium.

### *Encapsulation*

As the name implies, **encapsulation** is used to coat wastes with an impervious material so that they do not contact their surroundings. For example, a water-soluble waste salt encapsulated in asphalt would not dissolve so long as the asphalt layer remains intact. A common means of encapsulation uses heated, molten thermoplastics, asphalt, and waxes that solidify when cooled. A more sophisticated approach to encapsulation is to form polymeric resins from monomeric substances in the presence of the waste.

### **Chemical Fixation**

**Chemical fixation** is a process that binds a hazardous-waste substance in a less mobile, less toxic form by a chemical reaction that alters the waste chemically. Physical and chemical fixation often occur together, and sometimes it is a little difficult to distinguish between them. Polymeric inorganic silicates containing some calcium and often some aluminum are the inorganic materials most widely used as a fixation matrix. Many kinds of heavy metals are chemically bound in such a matrix, as well as being held physically by it. Similarly, some organic wastes are bound by reactions with matrix constituents.

## **22.11 ULTIMATE DISPOSAL OF WASTES**

Regardless of the destruction, treatment, and immobilization techniques used, there will always remain from hazardous wastes some material that has to be put somewhere. This section briefly addresses the ultimate disposal of ash, salts, liquids, solidified liquids, and other residues that must be placed where their potential to do harm is minimized.

## Disposal Above Ground

In some important respects disposal above ground, essentially in a pile designed to prevent erosion and water infiltration, is the best way to store solid wastes. Perhaps its most important advantage is that it avoids infiltration by groundwater that can result in leaching and groundwater contamination common to storage in pits and landfills. In a properly designed above-ground disposal facility, any leachate that is produced drains quickly by gravity to the leachate collection system, where it can be detected and treated.

Aboveground disposal can be accomplished with a storage mound deposited on a layer of compacted clay covered with impermeable membrane liners laid somewhat above the original soil surface and shaped to allow leachate flow and collection. The slopes around the edges of the storage mound should be sufficiently great to allow good drainage of precipitation, but gentle enough to deter erosion.

## Landfill

**Landfill** historically has been the most common way of disposing of solid hazardous wastes and some liquids, although it is being severely limited in many nations by new regulations and high land costs. Landfill involves disposal that is at least partially underground in excavated cells, quarries, or natural depressions. Usually fill is continued above ground to utilize space most efficiently and provide a grade for drainage of precipitation.

The greatest environmental concern with landfill of hazardous wastes is the generation of leachate from infiltrating surface water and groundwater with resultant contamination of groundwater supplies. Modern hazardous-waste landfills provide elaborate systems to contain, collect, and control such leachate.

There are several components to a modern landfill. A landfill should be placed on a compacted, low-permeability medium, preferably clay, which is covered by a flexible-membrane liner consisting of watertight impermeable material. This liner is covered with granular material in which is installed a secondary drainage system. Next is another flexible-membrane liner, above which is installed a primary drainage system for the removal of leachate. This drainage system is covered with a layer of granular filter medium, upon which the wastes are placed. In the landfill, wastes of different kinds are separated by berms consisting of clay or soil covered with liner material. When the fill is complete, the waste is capped to prevent surface water infiltration and covered with compacted soil. In addition to leachate collection, provision may be made for a system to treat evolved gases, particularly when methane-generating biodegradable materials are disposed in the landfill.

The flexible-membrane liner made of rubber (including chlorosulfonated polyethylene) or plastic (including chlorinated polyethylene, high-density polyethylene, and polyvinylchloride) is a key component of state-of-the-art landfills. It controls seepage out of, and infiltration into, the landfill. Obviously, liners must meet stringent standards to serve their intended purpose. In addition to being impermeable, the liner material must be strongly resistant to biodegradation, chemical attack, and tearing.

**Capping** is done to cover the wastes, prevent infiltration of excessive amounts of surface water, and prevent release of wastes to overlying soil and the atmosphere.



Caps come in a variety of forms and are often multilayered. Some of the problems that may occur with caps are settling, erosion, ponding, damage by rodents, and penetration by plant roots.

## **Surface Impoundment of Liquids**

Many liquid hazardous wastes, slurries, and sludges are placed in **surface impoundments**, which usually serve for treatment and often are designed to be filled in eventually as landfill disposal sites. Most liquid hazardous wastes and a significant fraction of solids are placed in surface impoundments in some stage of treatment, storage, or disposal.

A surface impoundment may consist of an excavated “pit,” a structure formed with dikes, or a combination thereof. The construction is similar to that discussed above for landfills in that the bottom and walls should be impermeable to liquids and provision must be made for leachate collection. The chemical and mechanical challenges to liner materials in surface impoundments are severe so that proper geological siting and construction with floors and walls composed of low-permeability soil and clay are important in preventing pollution from these installations.

## **Deep-Well Disposal of Liquids**

**Deep-well disposal** of liquids consists of their injection under pressure to underground strata isolated by impermeable rock strata from aquifers. Early experience with this method was gained in the petroleum industry where disposal is required of large quantities of saline wastewater coproduced with crude oil. The method was later extended to the chemical industry for the disposal of brines, acids, heavy metal solutions, organic liquids, and other liquids.

A number of factors must be considered in deep-well disposal. Wastes are injected into a region of elevated temperature and pressure, which may cause chemical reactions to occur involving the waste constituents and the mineral strata. Oils, solids, and gases in the liquid wastes can cause problems such as clogging. Corrosion may be severe. Microorganisms may have some effects. Most problems from these causes can be mitigated by proper waste pretreatment.

The most serious consideration involving deep-well disposal is the potential contamination of groundwater. Although injection is made into permeable saltwater aquifers presumably isolated from aquifers that contain potable water, contamination may occur. Major routes of contamination include fractures, faults, and other wells. The disposal well itself can act as a route for contamination if it is not properly constructed and cased or if it is damaged.

## **22.12 LEACHATE AND GAS EMISSIONS**

### **Leachate**

The production of contaminated leachate is a possibility with most disposal sites. Therefore, new hazardous-waste landfills require leachate collection/treatment systems and many older sites are required to have such systems retrofitted to them.

Modern hazardous-waste landfills typically have dual leachate collection systems, one located between the two impermeable liners required for the bottom and sides of the landfill, and another just above the top liner of the double-liner system. The upper leachate collection system is called the primary leachate collection system, and the bottom is called the secondary leachate collection system. Leachate is collected in perforated pipes that are embedded in granular drain material.

Chemical and biochemical processes have the potential to cause some problems for leachate collection systems. One such problem is clogging by insoluble manganese(IV) and iron(III) hydrated oxides upon exposure to air as described for water wells in Section 15.9.

Leachate consists of water that has become contaminated by wastes as it passes through a waste-disposal site. It contains waste constituents that are soluble, not retained by soil, and not degraded chemically or biochemically. Some potentially harmful leachate constituents are products of chemical or biochemical transformations of wastes.

The best approach to leachate management is to prevent its production by limiting infiltration of water into the site. Rates of leachate production may be very low when sites are selected, designed, and constructed with minimal production of leachate as a major objective. A well-maintained, low-permeability cap over the landfill is very important for leachate minimization.

## **Hazardous-Waste Leachate Treatment**

The first step in treating leachate is to characterize it fully, particularly with a thorough chemical analysis of possible waste constituents and their chemical and metabolic products. The biodegradability of leachate constituents should also be determined.

The options available for the treatment of hazardous-waste leachate are generally those that can be used for industrial wastewaters. These include biological treatment by an activated sludge or related process, and sorption by activated carbon, usually in columns of granular activated carbon. Hazardous-waste leachate can be treated by a variety of chemical processes, including acid-base neutralization, precipitation, and oxidation-reduction. In some cases, these treatment steps must precede biological treatment; for example, leachate exhibiting extremes of pH must be neutralized for microorganisms to thrive in it. Cyanide in the leachate can be oxidized with chlorine and organics with ozone, hydrogen peroxide promoted with ultraviolet radiation, or dissolved oxygen at high temperatures and pressures. Heavy metals can be precipitated with base, carbonate, or sulfide.

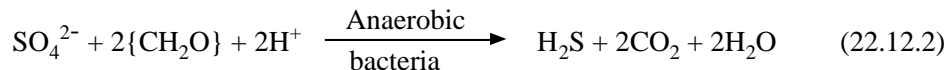
Leachate can be treated by a variety of physical processes. In some cases, simple density separation and sedimentation can be used to remove water-immiscible liquids and solids. Filtration is frequently required and flotation can be useful. Leachate solutes can be concentrated by evaporation, distillation, and membrane processes, including reverse osmosis, hyperfiltration, and ultrafiltration. Organic constituents can be removed from leachate by solvent extraction, air stripping, or steam stripping. In the case of volatile organic compounds in leachate (VOCs), care must be exercised to prevent excessive escape to the atmosphere, thus creating an air pollution problem as the result of leachate treatment.

## Gas Emissions

In the presence of biodegradable wastes, methane and carbon dioxide gases are produced in landfills by anaerobic degradation (see Reaction 22.8.1). Gases can also be produced by chemical processes with improperly pretreated wastes, as would occur in the hydrolysis of calcium carbide to produce acetylene:



Odorous and toxic hydrogen sulfide,  $\text{H}_2\text{S}$ , can be generated by the chemical reaction of sulfides with acids or by the biochemical reduction of sulfate by anaerobic bacteria (*Desulfovibrio*) in the presence of biodegradable organic matter:



Gases such as these may be toxic, combustible, or explosive. Furthermore, gases permeating through landfilled hazardous waste may carry along waste vapors, such as those of volatile aryl compounds and low-molar-mass halogenated hydrocarbons. Of these, the ones of most concern are benzene, 1,2-dibromoethane, 1,2-dichloroethane, carbon tetrachloride, chloroform, dichloromethane, tetrachloroethane, 1,1,1-trichloroethane, trichloroethylene, and vinyl chloride. Because of the hazards from these and other volatile species, it is important to minimize production of gases and, if significant amounts of gases are produced, they should be vented or treated by activated carbon sorption or flaring.

### 22.13 *IN-SITU* TREATMENT

*In-situ* treatment refers to waste treatment processes that can be applied to wastes in a disposal site by direct application of treatment processes and reagents to the wastes. Where possible, *in-situ* treatment is desirable for waste site remediation.

#### In-Situ Immobilization

*In-situ* immobilization is used to convert wastes to insoluble forms that will not leach from the disposal site. Heavy metal contaminants including lead, cadmium, zinc, and mercury, can be immobilized by chemical precipitation as the sulfides by treatment with gaseous  $\text{H}_2\text{S}$  or alkaline  $\text{Na}_2\text{S}$  solution. Disadvantages include the high toxicity of  $\text{H}_2\text{S}$  and the contamination potential of soluble sulfide. Although precipitated metal sulfides should remain as solids in the anaerobic conditions of a landfill, unintentional exposure to air can result in oxidation of the sulfide and remobilization of the metals as soluble sulfate salts.

Oxidation and reduction reactions can be used to immobilize heavy metals *in-situ*. Oxidation of soluble  $\text{Fe}^{2+}$  and  $\text{Mn}^{2+}$  to their insoluble hydrous oxides,  $\text{Fe}_2\text{O}_3 \cdot x\text{H}_2\text{O}$  and  $\text{MnO}_2 \cdot x\text{H}_2\text{O}$ , respectively, can precipitate these metal ions and coprecipitate other heavy-metal ions. However, subsurface reducing conditions could later result in reformation of soluble reduced species. Reduction can be used *in situ* to convert soluble, toxic chromate to insoluble chromium(III) compounds.

Chelation can convert metal ions to less mobile forms, although with most agents, chelation has the opposite effect. A chelating agent called Tetran is supposed to form metal chelates that are strongly bound to clay minerals. The humin fraction of soil humic substances likewise immobilizes metal ions.

## **Vapor Extraction**

Many important wastes have relatively high vapor pressures and can be removed by vapor extraction. This technique works for wastes in soil above the level of groundwater, that is, in the vadose zone. Simple in concept, vapor extraction involves pumping air into injection wells in soil and withdrawing it, along with volatile components that it has picked up, through extraction wells. The substances vaporized from the soil are removed by activated carbon or by other means. In some cases, the air is pumped through an engine (which can be used to run the air pumps) and are destroyed by conditions in the engine's combustion chambers. It is relatively efficient compared with groundwater pumping because of the much higher flow rates of air through soil compared with water. Vapor extraction is most applicable to the removal of volatile organic compounds (VOCs) such as chloromethanes, chloroethanes, chloroethylenes (such as trichloroethylene), benzene, toluene, and xylene.

## **Solidification InSitu**

*In-situ* solidification can be used as a remedial measure at hazardous-waste sites. One approach is to inject soluble silicates followed by reagents that cause them to solidify. For example, injection of soluble sodium silicate followed by calcium chloride or lime forms solid calcium silicate.

## **Detoxification In Situ**

When only one or a limited number of harmful constituents is present in a waste-disposal site, it may be practical to consider detoxification *in-situ*. This approach is most practical for organic contaminants including pesticides (organophosphate esters and carbamates), amides, and esters. Among the chemical and biochemical processes that can detoxify such materials are chemical and enzymatic oxidation, reduction, and hydrolysis. Chemical oxidants that have been proposed for this purpose include hydrogen peroxide, ozone, and hypochlorite.

Enzyme extracts collected from microbial cultures and purified have been considered for *in-situ* detoxification. One cell-free enzyme that has been used for detoxification of organophosphate insecticides is parathion hydrolase. The hostile environment of a chemical-waste landfill, including the presence of enzyme-inhibiting heavy-metal ions, is detrimental to many biochemical approaches to *in-situ* treatment. Furthermore, most sites contain a mixture of hazardous constituents, which might require several different enzymes for their detoxification.

## **Permeable-Bed Treatment**

Some groundwater plumes contaminated by dissolved wastes can be treated by a permeable bed of material placed in a trench through which the groundwater must

flow. Limestone in a permeable bed neutralizes acid and precipitates some heavy metal hydroxides or carbonates. Synthetic ion exchange resins can be used in a permeable bed to retain heavy metals and even some anionic species, although competition with ionic species present naturally in the groundwater can cause some problems with their use. Activated carbon in a permeable bed will remove some organics, especially less soluble, higher molar mass organic compounds.

Permeable-bed treatment requires relatively large quantities of reagent, which argues against the use of activated carbon and ion exchange resins. In such an application it is unlikely that either of these materials could be reclaimed and regenerated as is done when they are used in columns to treat wastewater. Furthermore, ions taken up by ion exchangers and organic species retained by activated carbon may be released at a later time, causing subsequent problems. Finally, a permeable bed that has been truly effective in collecting waste materials may, itself, be considered a hazardous waste requiring special treatment and disposal.

### **In-Situ Thermal Processes**

Heating of wastes *in situ* can be used to remove or destroy some kinds of hazardous substances. Steam injection and radio frequency and microwave heating have been proposed for this purpose. Volatile wastes brought to the surface by heating can be collected and held as condensed liquids or by activated carbon.

One approach to immobilizing wastes *in-situ* is high temperature vitrification using electrical heating. This process involves pouring conducting graphite on the surface between two electrodes and passing an electric current between the electrodes. In principle, the graphite becomes very hot and “melts” into the soil, leaving a glassy slag in its path. Volatile species evolved are collected and, if the operation is successful, a nonleachable slag is left in place. It is easy to imagine problems that might occur, including difficulties in getting a uniform melt, problems from groundwater infiltration, and very high consumption of electricity.

### **Soil Washing and Flushing**

Extraction with water containing various additives can be used to cleanse soil contaminated with hazardous wastes. When the soil is left in place and the water pumped into and out of it, the process is called **flushing**; when soil is removed and contacted with liquid the process is referred to as **washing**. Here, washing is used as a term applied to both processes.

The composition of the fluid used for soil washing depends upon the contaminants to be removed. The washing medium may consist of pure water or it may contain acids (to leach out metals or neutralize alkaline soil contaminants), bases (to neutralize contaminant acids), chelating agents (to solubilize heavy metals), surfactants (to enhance the removal of organic contaminants from soil and improve the ability of the water to emulsify insoluble organic species), or reducing agents (to reduce oxidized species). Soil contaminants may dissolve, form emulsions, or react chemically. Heavy metal salts; lighter aromatic hydrocarbons, such as toluene and xylenes; lighter organohalides, such as trichloro- or tetrachloroethylene; and light-to-medium molar mass aldehydes and ketones can be removed from soil by washing.

## CHAPTER SUMMARY

*The chapter summary below is presented in a programmed format to review the main points covered in this chapter. It is used most effectively by filling in the blanks, referring back to the chapter as necessary. The correct answers are given at the end of the summary.*

In descending order of desirability, the five objectives of hazardous-waste management are <sup>1</sup> \_\_\_\_\_

\_\_\_\_\_  
\_\_\_\_\_  
\_\_\_\_\_.

The **effectiveness** of a hazardous-waste management system is a measure of <sup>2</sup> \_\_\_\_\_

\_\_\_\_\_.  
By its nature, a system of industrial ecology is also a system of waste \_\_\_\_\_  
\_\_\_\_\_. Cutting down quantities of wastes from their  
sources is known as <sup>3</sup> \_\_\_\_\_ and utilization of treatment  
processes that reduce the quantities of wastes requiring ultimate disposal is called  
<sup>4</sup> \_\_\_\_\_. The most effective approach to minimizing  
wastes is to emphasize <sup>5</sup> \_\_\_\_\_

\_\_\_\_\_. A crucial part of the process for  
reducing and minimizing wastes is the development of a <sup>6</sup> \_\_\_\_\_ balance.

The four broad areas in which something of value can be obtained from recycling  
wastes are <sup>7</sup> \_\_\_\_\_

\_\_\_\_\_  
\_\_\_\_\_  
\_\_\_\_\_.

Some of the more important examples of substances recycled are <sup>8</sup> \_\_\_\_\_

\_\_\_\_\_  
\_\_\_\_\_.

Annual production of potentially recyclable waste oil in the United States is  
approximately <sup>9</sup> \_\_\_\_\_, of which around half is <sup>10</sup> \_\_\_\_\_

\_\_\_\_\_. Waste oil that is to be used for fuel is given <sup>11</sup> \_\_\_\_\_  
treatment of a <sup>12</sup> \_\_\_\_\_ nature. The most important operation in solvent  
purification and recycling is <sup>13</sup> \_\_\_\_\_. Two of the major potential  
pollution problems with industrial water recycling are <sup>14</sup> \_\_\_\_\_

\_\_\_\_\_. Although wastewater distillation, treatment with activated  
carbon, reverse osmosis, and other treatment processes produce very high quality  
water for recycling they have the disadvantage of <sup>15</sup> \_\_\_\_\_

\_\_\_\_\_. Waste treatment can occur at the three major levels of <sup>16</sup> \_\_\_\_\_  
\_\_\_\_\_. Major categories of physical waste  
treatment include <sup>17</sup> \_\_\_\_\_

\_\_\_\_\_. Means of separation of components of  
a waste mixture that are already in two different phases include <sup>18</sup> \_\_\_\_\_

Physical separation by phase transition is best exemplified by <sup>19</sup>\_\_\_\_\_, a potential waste problem resulting from which is production of <sup>20</sup>\_\_\_\_\_. Common means of removing solvent from a waste, other than distillation are <sup>21</sup>\_\_\_\_\_. Separating volatile components from less volatile ones in a liquid mixture by the partitioning of the more volatile materials to a gas phase of air or steam is called <sup>22</sup>\_\_\_\_\_. Physical precipitation describes <sup>23</sup>\_\_\_\_\_. An important example of phase transfer involving two liquids and at least one solute is <sup>24</sup>\_\_\_\_\_. The most common supercritical fluid used for extraction is <sup>25</sup>\_\_\_\_\_. Transfer of a substance from a solution to a solid phase is called <sup>26</sup>\_\_\_\_\_ and the most common sorbent, especially for organic compounds, is <sup>27</sup>\_\_\_\_\_. Molecular separation is often based upon <sup>28</sup>\_\_\_\_\_, of which the most widely used is <sup>29</sup>\_\_\_\_\_. The chemical properties of constituents of a waste that generally determine the kind of chemical treatment to which it may be subjected are <sup>30</sup>\_\_\_\_\_.

Common unit operations in chemical treatment of wastes are <sup>31</sup>\_\_\_\_\_. Waste acids and bases are treated by <sup>32</sup>\_\_\_\_\_. Chemical precipitation is used in hazardous-waste treatment primarily for the removal of <sup>33</sup>\_\_\_\_\_ from water. Some metals can be precipitated from solution in the elemental metal form by the action of <sup>34</sup>\_\_\_\_\_. Displacement from solution into the elemental state of a dissolved hazardous metal through the action of a nonhazardous elemental metal is a treatment process called <sup>35</sup>\_\_\_\_\_. A strong oxidant that can be generated on-site by an electrical discharge through dry air or oxygen then used for waste treatment is <sup>36</sup>\_\_\_\_\_. Electrolysis is a waste-treatment process in which <sup>37</sup>\_\_\_\_\_.

A chemical waste treatment process that could be used to treat metal hydrides, alkoxides, nonmetal oxyhalides, and organic anhydrides is <sup>38</sup>\_\_\_\_\_. Reducing agents might be used to treat soils to remove <sup>39</sup>\_\_\_\_\_. Cations or anions are removed from solution onto a solid resin, which can be regenerated by treatment with acids, bases, or salts through a process called <sup>40</sup>\_\_\_\_\_. In waste treatment, photochemical reactions are used for <sup>41</sup>\_\_\_\_\_. In some cases where photochemical means are used for waste treatment, sensitizers are added to the reaction mixture to <sup>42</sup>\_\_\_\_\_.

\_\_\_\_\_ . A process that utilizes high temperatures, an oxidizing atmosphere, and often turbulent combustion conditions to destroy wastes is <sup>43</sup> \_\_\_\_\_. The two most widely used types of hazardous-waste incinerators are <sup>44</sup> \_\_\_\_\_. Effectiveness of incineration is measured by destruction of the <sup>45</sup> \_\_\_\_\_ and expressed as <sup>46</sup> \_\_\_\_\_. United States EPA regulations call for destruction/removal of <sup>47</sup> \_\_\_\_\_ percent of POHCs and <sup>48</sup> \_\_\_\_\_ percent of 2,3,7,8-tetrachlorodibenzo-*p*-dioxin. Wet air oxidation involves <sup>49</sup> \_\_\_\_\_, a process that can be enhanced by <sup>50</sup> \_\_\_\_\_. The use of microbial processes to destroy hazardous wastes is called <sup>51</sup> \_\_\_\_\_. Hazardous-waste substances that resist biodegradation are termed <sup>52</sup> \_\_\_\_\_. Aerobic waste treatment utilizes bacteria and or fungi that require <sup>53</sup> \_\_\_\_\_. The overall process for anaerobic digestion of wastes is a <sup>54</sup> \_\_\_\_\_ process in which organic matter is both <sup>55</sup> \_\_\_\_\_. Reductive dehalogenation is a mechanism by which <sup>56</sup> \_\_\_\_\_ are removed from organohalide compounds by the action of <sup>57</sup> \_\_\_\_\_. Land treatment of wastes may be accomplished by <sup>58</sup> \_\_\_\_\_. Composting of hazardous wastes is the biodegradation of solid or solidified materials <sup>59</sup> \_\_\_\_\_. Immobilization of wastes includes physical and chemical processes that <sup>60</sup> \_\_\_\_\_. Stabilization means conversion of waste to a form that is less likely to be <sup>61</sup> \_\_\_\_\_ after disposal. For solidifying and stabilizing organic wastes a good solid sorbent to use is <sup>62</sup> \_\_\_\_\_. For disposal, hazardous-waste materials can be mixed with hot <sup>63</sup> \_\_\_\_\_ liquids and solidified in the cooled <sup>64</sup> \_\_\_\_\_ matrix, which is rigid but deformable. Vitrification consists of imbedding wastes in a <sup>65</sup> \_\_\_\_\_ material. A common construction material used to solidify hazardous wastes for disposal is <sup>66</sup> \_\_\_\_\_. Pozzolanic substances used for waste disposal consist of <sup>67</sup> \_\_\_\_\_. Chemical fixation is a process that binds a hazardous-waste substance in a less mobile, less toxic form by <sup>68</sup> \_\_\_\_\_. Historically, <sup>69</sup> \_\_\_\_\_ has been the most common way of disposing of solid hazardous wastes and some liquids. The greatest potential problem with this means of waste disposal is <sup>70</sup> \_\_\_\_\_. Injection of wastes into underground strata isolated by impermeable rock strata from aquifers is referred to as <sup>71</sup> \_\_\_\_\_. The most common water pollution problem arising from waste disposal is <sup>72</sup> \_\_\_\_\_ and the most common air pollution problem is <sup>73</sup> \_\_\_\_\_. Treating wastes in place in the ground is referred to as <sup>74</sup> \_\_\_\_\_. Excavation down to a plume of waste flow underground and placing a substance for treatment in the path of the plume is known as <sup>75</sup> \_\_\_\_\_. Treating contaminated soil left in place by pumping water into and out of it is a



process called <sup>76</sup> \_\_\_\_\_; when soil is removed and contacted with liquid the process is referred to as <sup>77</sup> \_\_\_\_\_.

### *Answers to Chapter Summary*

1. (1) do not produce it, (2) if making it cannot be avoided, produce only minimum quantities, (3) recycle it, (3) if it is produced and cannot be recycled, treat it, preferably in a way that makes it nonhazardous, (4) if it cannot be rendered nonhazardous, dispose of it in a safe manner, (5) once it is disposed of, monitor it for leaching and other adverse effects
2. how well it reduces the quantities and hazards of wastes
3. waste reduction
4. waste minimization
5. waste minimization as an integral part of plant design
6. material
7. (1) direct recycle as raw material to the generator, as with the return to feedstock of raw materials not completely consumed in a synthesis process, (2) transfer as a raw material to another process; a substance that is a waste product from one process may serve as a raw material for another, sometimes in an entirely different industry, (3) utilization for pollution control or waste treatment, such as use of waste alkali to neutralize waste acid, (4) recovery of energy, for example, from the incineration of combustible hazardous wastes.
8. ferrous metals, nonferrous metals, metal compounds, inorganic substances, glass, paper, plastic, rubber, organic substances, catalysts, and materials with agricultural uses
9. 4 billion liters
10. burned as fuel
11. minimal
12. physical
13. fractional distillation
14. heavy metals and dissolved toxic organic species
15. producing potentially hazardous byproducts
16. primary, secondary, and polishing
17. phase separation, phase transfer, phase transition, and membrane separations
18. sedimentation and decanting, filtration, centrifugation, flotation
19. distillation
20. distillation bottoms
21. evaporation, including thin-film evaporation, and drying, including freeze drying
22. stripping
23. processes in which a solid forms from a solute in solution as a result of a physical change in the solution
24. solvent extraction
25. carbon dioxide
26. sorption
27. activated carbon
28. membrane processes
29. reverse osmosis

30. acid-base, oxidation-reduction, precipitation, and complexation behavior; reactivity; flammability/combustibility; corrosivity; and compatibility with other wastes
31. acid-base neutralization, chemical precipitation, chemical extraction and leaching, oxidation, reduction, and ion exchange
32. neutralization
33. heavy-metal ions
34. a reducing agent such as sodium borohydride
35. cementation
36. ozone
37. one species in solution (usually a metal ion) is reduced by electrons at the cathode and another gives up electrons to the anode and is oxidized there
38. hydrolysis, the reaction with water
39. heavy metals coprecipitated with  $\text{Fe}_2\text{O}_3$  or  $\text{MnO}_2$
40. ion exchange
41. breaking chemical bonds in refractory organic compounds
42. absorb radiation and generate reactive species that destroy wastes
43. incineration
44. rotary kiln and liquid injection
45. principal organic hazardous constituents
46. destruction removal efficiency
47. 99.99
48. 99.9999
49. oxidizing wastes in water at high temperatures and very high pressures
50. ultraviolet radiation
52. refractory or recalcitrant
53. molecular oxygen
54. fermentation
55. oxidized and reduced
56. halogen atoms
57. anaerobic bacteria
58. mixing the wastes with soil under appropriate conditions
59. in a medium other than soil
60. reduce surface areas of wastes to minimize leaching
61. mobile
62. activated carbon
63. thermoplastic
64. thermoplastic
65. glass
66. Portland cement
67. water-insoluble silicates
68. a chemical reaction that alters the waste chemically
69. landfill
70. production of leachate that may contaminate groundwater
71. deep well disposal
72. production of leachate
73. release of gases
74. *in-situ* treatment

75. permeable-bed treatment
76. soil flushing
77. soil washing

## LITERATURE CITED

1. Hileman, Bette, "Another Stab at Superfund Reform," *Chemical and Engineering News*, June 28, 1999, pp. 20-21.
2. Jandrasi, Frank J. and Stephen Z. Masoomian, "Process Waste During Plant Design," *Environmental Engineering World*, **1**, 6-15 (1995).
3. Ray, Chittaranjan, Ravi K. Jain, Bernard A. Donahue, and E. Dean Smith, "Hazardous Waste Minimization Through Life Cycle Cost Analysis at Federal Facilities," *Journal of the Air and Waste Management Association*, **49**, 17-27 (1999).
4. Hall, Freddie E., Jr. , "OC-ALC Hazardous Waste Minimization Strategy: Reduction of Industrial Biological Sludge from Industrial Wastewater Treatment Facilities," *Proceedings of the Annual Meeting of the Air Waste Management Association*, **90**, 1052-6102 (1997).
5. Smith, Edward H. and Carlos Davis, "Hazardous Materials Balance Approach for Source Reduction and Waste Minimization," *Journal of Environmental Science and Health, Part A.*, **32**, 171-193 (1997).
6. Richardson, Kelly E. and Terry Bursztynsky, "Refinery Waste Minimization," *Proceedings of HAZMACON 95*, 505-513 (1995).
7. Eckenfelder, W. Wesley, Jr. and A. H. Englande, Jr., "Chemical/Petrochemical Wastewater Management—Past, Present and Future," *Water Science Technology*, **34**, 1-7 (1996).
8. Ellis, Jeffrey I., "Waste Water Recycling and Pre-treatment Systems: an Alternative to Oil/Water Separators," *Proceedings of the Annual Meeting of the Air Waste Management Association*, **91**, 1052-6102 (1998).
9. Chang, Li-Yang, "A Waste Minimization Study of a Chelated Copper Complex in Wastewater—Treatability and Process Analysis," *Waste Management (New York)*, **15**, 209-20 (1995).
10. Macchi, G., M. Pagano, M. Santori, and G. Tiravanti, "Battery Industry Wastewater: Pb Removal and Produced Sludge," *Water Research*, **27**, 1511-1518 (1993).
11. Abda, Moshe and Yoram Oren, "Removal of Cadmium and Associated Contaminants from Aqueous Wastes by Fibrous Carbon Electrodes" *Water Research*, **27**, 1535-1544 (1993).
12. Paul, S. F., "Review of Thermal Plasma Research and Development for Hazardous Waste Remediation in the United States," *Thermal Plasmas for Hazardous Waste Treatment, Proceedings of the International Symposium on*

*Plasma Physics "Piero Caldirola,"* Roberto Benocci, Giovanni Bonizzoni, and Elio Sindoni, Eds., World Scientific, Singapore, 1996, pp. 67-92.

13. Mohn, William W., and James M. Tiedje, "Microbial Reductive Dehalogenation," *Microbial Reviews*, **56**, 482-507 (1992).

## **SUPPLEMENTARY REFERENCES**

ACS Task Force on Laboratory Waste Management, *Laboratory Waste Management: A Guidebook*, American Chemical Society, Washington, D.C., 1994.

Anderson, Todd A. and Joel R. Coats, Eds., *Bioremediation Through Rhizosphere Technology*, American Chemical Society, Washington, D.C., 1994.

Anderson, W. C., *Innovative Site Remediation Technology*, Springer-Verlag, New York, 1995.

Armour, Margaret-Ann, *Hazardous Laboratory Chemicals Disposal Guide*, CRC Press/Lewis Publishers, Boca Raton, FL, 1996.

Barth, Edwin F., *Stabilization and Solidification of Hazardous Wastes* (Pollution Technology Review, No 186), Noyes Publications, Park Ridge, NJ, 1990.

Bentley, S. P., Ed., *Engineering Geology of Waste Disposal*, American Association of Petroleum Geologists, Houston, TX, 1995.

Bierma, Thomas J. and Frank L. Waterstraat, *Waste Minimization through Shared Savings: Chemical Supply Strategies*, John Wiley & Sons, New York, 1999.

Boardman, Gregory D., Ed., *Proceedings of the Twenty-Ninth Mid-Atlantic Industrial and Hazardous Waste Conference*, Technomic Publishing Co., Lancaster, PA, 1997.

Bodocsi, A., Michael E. Ryan, and Ralph R. Rumer, Eds., *Barrier Containment Technologies for Environmental Remediation Applications*, John Wiley & Sons, New York, 1995.

Cheremisinoff, Nicholas P., *Groundwater Remediation and Treatment Technologies*, Noyes Publications, Westwood, NJ, 1998.

Cheremisinoff, Nicholas P., *Biotechnology for Waste and Wastewater Treatment*, Noyes Publications, Park Ridge, NJ, 1996.

Cheremisinoff, Paul N., *Waste Minimization and Cost Reduction for the Process Industries*, Noyes Publications, Park Ridge, NJ, 1995.

Childers, Darin G., *Environmental Economics: Profiting from Waste Minimization: A Practical Guide to Achieving Improvements in Quality, Profitability, and Competitiveness through the Prevention of Pollution*, Water Environment Federation, Alexandria, VA, 1998.

Ciambrone, David F., *Waste Minimization As a Strategic Weapon*, CRC Press/Lewis Publishers, Boca Raton, FL, 1996.

Clark, J. H., Ed., *Chemistry of Waste Minimization*, Blackie Academic and Professional, New York, 1995.

- Davis, John W., *Fast Track to Waste-Free Manufacturing: Straight Talk from a Plant Manager*, Productivity Press, Portland, OR, 1999.
- Epps, John A. and Chin-Fu Tsang, Eds., *Industrial Waste: Scientific and Engineering Aspects*, Academic Press, San Diego, CA, 1996.
- Freeman, Harry and Eugene F. Harris, Eds., *Hazardous Waste Remediation: Innovative Treatment Technologies*, Technomic Publishing Co., Lancaster, PA, 1995.
- Frosch, Robert A., "Industrial Ecology: Adapting Technology for a Sustainable World," *Environment Magazine*, **37**, 16–37, 1995.
- Gilliam, Michael T. and Carlton G. Wiles, Eds., *Stabilization and Solidification of Hazardous, Radioactive, and Mixed Wastes* (ASTM Special Technical Publication, 1123), American Society for Testing and Materials, Philadelphia, 1992.
- Graedel, Thomas E. and B. R. Allenby, "Industrial Process Residues: Composition and Minimization," Chapter 15 in *Industrial Ecology*, Prentice Hall, Englewood Cliffs, NJ, 1995, pp. 204–230.
- Haas, Charles N. and Richard J. Vamos, *Hazardous and Industrial Waste Treatment*, Prentice Hall Press, New York, 1995.
- Hester, R. E., and R. M. Harrison, *Waste Treatment and Disposal* (Issues in Environmental Science and Technology, 3), Royal Society of Chemistry, London, 1995.
- Hickey, Robert F. and Gretchen Smith, Eds., *Biotechnology in Industrial Waste Treatment and Bioremediation*, CRC Press/Lewis Publishers, Boca Raton, FL, 1996.
- Hinchee, Robert E., Rodney S. Skeen, and Gregory D. Sayles, *Biological Unit Processes for Hazardous Waste Treatment*, Battelle Press, Columbus, OH 1995.
- International Atomic Energy Agency Vienna, *Minimization of Radioactive Waste from Nuclear Power Plants and the Back End of the Nuclear Fuel Cycle*, International Atomic Energy Agency, Vienna, 1995.
- Karnofsky, Brian, Ed., *Hazardous Waste Management Compliance Handbook*, 2nd ed., Van Nostrand Reinhold, New York, 1996.
- LaGrega, Michael D., Phillip L. Buckingham, and Jeffrey C. Evans, *Hazardous Waste Management*, McGraw-Hill, New York, 1994.
- Long, Robert B., *Separation Processes in Waste Minimization*, Marcel Dekker, New York, 1995.
- Lewandowski, Gordon A. and Louis J. DeFilippi, *Biological Treatment of Hazardous Wastes*, John Wiley & Sons, New York, 1997.
- National Research Council, *Review and Evaluation of Alternative Chemical Disposal Technologies*, National Academy Press, Washington, D.C., 1997.
- Nemorow, Nelson, *Zero Pollution for Industry : Waste Minimization Through Industrial Complexes*, John Wiley & Sons, New York, 1995.

- Olsen, Scott, Barbara J. McKellar, and Kathy Kuntz, *Enhancing Industrial Competitiveness: First Steps to Recognizing the Potential of Energy Efficiency and Waste Minimization*, Wisconsin Demand-Side Demonstrations, Inc., Madison, WI, 1995.
- Reed, Sherwood C., Ronald W. Crites, and E. Joe Middlebrooks, *Natural Systems for Waste Management and Treatment*, McGraw-Hill, New York, 1995.
- Reinhardt, Peter A., K. Leigh Leonard, and Peter C. Ashbrook, Eds., *Pollution Prevention and Waste Minimization in Laboratories*, CRC Press/Lewis Publishers, Boca Raton, FL, 1996.
- Roberts, Stephen M., Christopher M. Teaf, and Judy A. Bean, Eds., *Hazardous Waste Incineration: Evaluating the Human Health and Environmental Risks*, CRC Press/Lewis Publishers, Boca Raton, FL, 1999.
- Rossiter, Alan P., Ed., *Waste Minimization Through Process Design*, McGraw-Hill, New York, 1995.
- Sellers, Kathleen, *Fundamentals of Hazardous Waste Site Remediation*, CRC Press/Lewis Publishers, Boca Raton, FL, 1999.
- Tedder, D. William and Frederick G. Pohland, Eds., *Emerging Technologies in Hazardous Waste Management 7*, Plenum, New York, 1997.
- Thomas, Suzanne T., *Facility Manager's Guide to Pollution Prevention and Waste Minimization*, BNA Books, Castro Valley, CA, 1995.
- Waste Characterization and Treatment*, Society for Mining Metallurgy & Exploration, Littleton, CO, 1998.
- Water and Residue Treatment*, Volume II, Hazardous Materials Control Research Institute, Silver Spring, MD, 1987.
- Watts, Richard J., *Hazardous Wastes: Sources, Pathways, Receptors*, John Wiley & Sons, New York, 1997.
- Williams, Paul T., *Waste Treatment and Disposal*, John Wiley & Sons, New York, 1998.
- Winkler, M. A., *Biological Treatment of Waste-Water*, Halsted Press (John Wiley & Sons), New York, 1997.
- Wise, Donald L., and Debra J. Trantolo, *Process Engineering for Pollution Control and Waste Minimization*, Marcel Dekker, Inc., New York, 1994.

## QUESTIONS AND PROBLEMS

1. Place the following in descending order of desirability for dealing with wastes and discuss your rationale for doing so: (a) reducing the volume of remaining wastes by measures such as incineration, (b) placing the residual material in landfills, properly protected from leaching or release by other pathways, (c) treating residual material as much as possible to render it nonleachable and innocuous, (d) reduction of wastes at the source, (e) recycling as much waste as is practical.

2. Match the waste-recycling process or industry from the column on the left with the kind of material that can be recycled from the list on the right, below:
- |   |   |
|---|---|
| 1. Recycle as raw material to the generator             | (a) Waste alkali                              |
| 2. Utilization for pollution control or waste treatment | (b) Hydraulic and lubricating oils            |
| 3. Energy production                                    | (c) Incinerable materials                     |
| 4. Materials with agricultural uses                     | (d) Incompletely consumed feedstock material  |
| 5. Organic substances                                   | (e) Waste lime or phosphate-containing sludge |
3. What material is recycled using hydrofinishing, treatment with clay, and filtration?
4. What is the “most important operation in solvent purification and recycle” that is used to separate solvents from impurities, water, and other solvents?
5. Dissolved air flotation (DAF) is used in the secondary treatment of wastes. What is the principle of this technique? For what kinds of hazardous-waste substances is it most applicable?
6. Match the process or industry from the column on the left with its “phase of waste treatment” from the list on the right, below:
- |                              |                         |
|------------------------------|-------------------------|
| 1. Activated carbon sorption | (a) Primary treatment   |
| 2. Precipitation             | (b) Secondary treatment |
| 3. Reverse osmosis           | (c) Polishing           |
| 4. Emulsion breaking         |                         |
| 5. Slurrying                 |                         |
7. Distillation is used in treating and recycling a variety of wastes, including solvents, waste oil, aqueous phenolic wastes, and mixtures of ethylbenzene and styrene. What is the major hazardous-waste problem that arises from the use of distillation for waste treatment?
8. Supercritical fluid technology has a great deal of potential for the treatment of hazardous wastes. What are the principles involved with the use of supercritical fluids for waste treatment? Why is this technique especially advantageous? Which substance is most likely to be used as a supercritical fluid in this application? For which kinds of wastes are supercritical fluids most useful?
9. What are some advantages of using acetic acid, compared, for example, with sulfuric acid, as a neutralizing agent for treating waste alkaline materials?
10. Which of the following would be **least likely** to be produced by, or used as a reagent for the removal of heavy metals by their precipitation from solution? (a)  $\text{Na}_2\text{CO}_3$ , (b)  $\text{CdS}$ , (c)  $\text{Cr}(\text{OH})_3$ , (d)  $\text{KNO}_3$ , (e)  $\text{Ca}(\text{OH})_2$
11. Both  $\text{NaBH}_4$  and  $\text{Zn}$  are used to remove metals from solution. How do these substances remove metals? What are the forms of the metal products?

12. Of the following, thermal treatment of wastes is **not** useful for (a) volume reduction, (b) destruction of heavy metals, (c) removal of volatile, combustible, mobile organic matter, (d) destruction of pathogenic materials, (e) destruction of toxic substances.
13. From the following, choose the waste liquid that is least amenable to incineration and explain why it is not readily incinerated: (a) methanol, (b) tetrachloroethylene, (c) acetonitrile, (d) toluene, (e) ethanol, (f) acetone.
14. Name and give the advantages of the process that is used to destroy more hazardous wastes by thermal means than are burned solely for the purpose of waste destruction.
15. What is the major advantage of fluidized-bed incinerators from the standpoint of controlling pollutant by-products?
16. What is the best way to obtain microorganisms to be used in the treatment of hazardous wastes by biodegradation?
17. What are the principles of composting? How is it used to treat hazardous wastes?
18. How is Portland cement used in the treatment of hazardous wastes for disposal? What might be some disadvantages of such a use?
19. What are the advantages of above ground disposal of hazardous wastes as opposed to burying wastes in landfills?
20. Describe and explain the best approach to managing leachate from hazardous-waste disposal sites.